1 # A fully coupled meso-scale electro-chemo-mechanical phase

2 # field method for corrosion-induced fracture in concrete

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10 **Abstract**

11 Corrosion-induced concrete cover deterioration is a major factor affecting the serviceability of the

12 reinforced concrete (RC) structures. The entire corrosion process, including mass transport,

13 physical/chemical/electrochemical reactions, and cover cracking, occurs at the meso-scale. This

14 paper developed a fully coupled meso-scale electro-chemo-mechanical phase field method to

15 accurately simulate the corrosion mechanism in RC structures. The simulation begins with the mass

16 transport process in the concrete, including the moisture, chloride ions and oxygen. When the

17 chloride concentration at the rebar surface reaches a critical value, corrosion initiates and then

18 propagates. A meso-scale phase field model is adopted for characterizing the corrosion-induced

19 damage in both mortar and interfacial transition zones (ITZs). In addition, crack direction dependent

20 diffusivity tensors are proposed to consider the influence of damage on the mass transport process.

21 The proposed numerical method is verified by previously reported experimental results, showing

22 the ability to conduct high-fidelity simulations of corrosion-induced fracture in RC structures.

23 Parametric studies are carried out to investigate the effect of aggregate distribution, cover thickness,

24 relative humidity, and temperature on the corrosion process.

25 **Keywords**: Corrosion modeling; Mass transport; Phase field method; Crack-dependent diffusivity

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1. Introduction

Chloride-induced corrosion is one of the primary causes for early age deterioration of reinforced concrete (RC) structures exposed to marine environments. Generally, the embedded rebar is protected from corrosion by a passive film formed due to the highly alkaline environment in the concrete. However, as external water and chloride ions penetrate into the concrete, the passive protective layer gets destroyed, leading to corrosion of steel reinforcement. Corrosion in the RC structure is a complex process comprising physical, chemical and electrochemical reactions. As rust expands, the hoop stress in the concrete surrounding the rebar reaches the material strength, leading to tensile cracks. Subsequently, the developed cracks allow further ingress of water, chloride ions and oxygen, accelerating the corrosion process until the concrete cover is completely damaged. Corrosion is a major threat to the safety of RC structures. Therefore, in the past few decades, a considerable amount of experimental work has been carried out on the corrosion and the corresponding deterioration of the concrete cover (Andrade et al., 1993, Cabrera, 1996, Alonso et al., 1998, Castel et al., 2000, Jaffer and Hansson, 2009, Wong et al., 2010, Fischer, 2012, Ye et al., 2017, Amalia et al., 2018). However, experiments under real environmental conditions often require prolonged investigation, making them labor intensive. In this regard, a high-fidelity simulation framework can be a powerful and promising alternative.

The overall chloride-induced corrosion process comprises chloride transport, the electrochemical reactions between steel rebar and chloride ions and the resulting corrosion leading to rust formation and cracking. These crack formations lead to premature fractures in RC structures, thus expediating early age repair. Over the years, many numerical studies have been carried out to analyze the corrosion-induced fracture in RC structures. In some studies, empirical corrosion- or time-dependent corrosion models characterizing the rust distributions are used to investigate the effects of material properties or the structural factors (e.g., cover depth, cover to rebar diameter ratio and multiple rebars) on the service life estimation (Jang and Oh, 2010, Tran et al., 2011, Zhao et al., 2011, Zhang et al., 2017, Xi and Yang, 2017, Cao et al., 2013, Cao and Cheung, 2014). However, the empirical corrosion models are usually obtained from a statistical point of view. It may not be able to accurately reflect the rust distribution under specific environmental conditions. Duan et al. (2015) presented a probabilistic model to estimate the risk of chloride penetration-induced corrosion

59   considering the time-dependent diffusion coefficient and surface chloride concentration. Wei et al.

60   (2021) developed a phase field model to simulate the corrosion-induced fracture of concrete with a

61   uniform rust distribution, in which the expansion of the rust was evaluated by an empirical

62   relationship with respect to the oxygen supply. Ožbolt et al. (2010) simulated oxygen, moisture and

63   chloride transport processes and the interaction between the mass transport and the damage in

64   concrete. However, the mass transport processes are not uniform and vary significantly with the

65   changes in environmental conditions (e.g., temperature and humidity). An in-depth assessment of

66   the temperature effect on corrosion risk was carried out by Pour-Ghaz et al. (2009a) using simulated

67   polarization resistance tests. Chauhan and Sharma (2021) studied non-uniform corrosion in RC

68   beams under realistic climate conditions and reported that variations in humidity and temperatures

69   affect the crack width and pattern. Therefore, it becomes utmost important to consider

70   environmental parameters in the corrosion model.

71   It is worth mentioning that most reported studies assumed concrete as a homogeneous material.

72   This helps to reduce computational efforts when dealing with large-scale problems. However, the

73   corrosion-induced cracks usually initiate near the rebar to concrete contact surface and are

74   significantly affected by the aggregate distribution. Hence, an accurate simulation of the corrosion

75   mechanism requires a meso-scale concrete model that treats the concrete as a multiple-phase

76   material of the mortar matrix, aggregates and interfacial transition zones (ITZs). Studies using meso-

77   scale models have been conducted to investigate the heterogenous corrosion-induced cracks in

78   concretes with different reinforcement cases (Du et al., 2014, Chen et al., 2018, Xi et al., 2018a, Xi

79   et al., 2018b). These studies only focused on the cracking of the concrete cover and implemented

80   the rust expansion using empirical functions. However, based on the previous research (Qiu and Dai,

81   2021) the concrete's heterogeneity as well as the internal meso-scale cracks will significantly affect

82   the mass transport process. This will subsequently affect the electrochemical reaction and the rust

83   generation on the rebar surface. Therefore, a more comprehensive meso-scale model that can

84   consider the entire process of the initiation and propagation of rebar corrosion is desired.
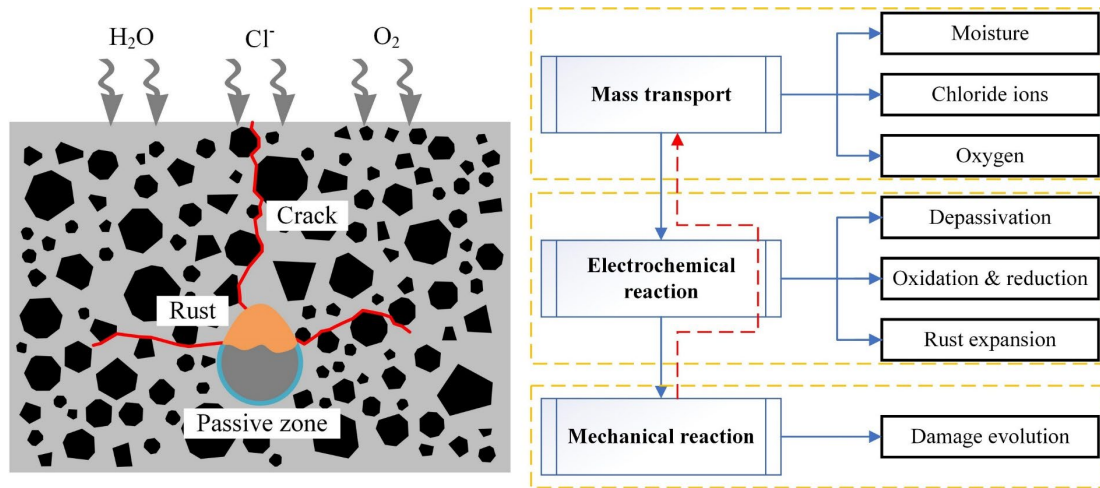
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Fig. 1. Illustration and flow chart of the proposed meso-scale electro-chemo-mechanical phase field method.

The present paper proposes a comprehensive meso-scale model simulating the RC structure's entire corrosion process. As shown in Fig. 1, the simulation consists of three main parts: mass transport, electrochemical reaction and mechanical reaction. Blue and red arrows represent the interaction between the different mechanisms. The mass transport processes of moisture, chloride ions and oxygen are first considered. When the chloride concentration at the rebar surface reaches a critical value, corrosion initiates and propagates with oxygen transported through the pore solution. During this period, both micro- and macro-cell corrosion mechanisms are considered to estimate the accumulation of the rust on the rebar surface. Since the rust density is smaller than the dissolved iron, the hoop stress around the rebar will become larger with rust expansion. This will lead to damage initiation near the rebar as the hoop stress reaches the material strength. In this study, the damage of the mortar and the ITZs is modeled by a meso-scale phase field model. Phase field model is kind of non-local smeared crack model based on the Francfort-Marigo variational principle (Francfort and Marigo, 1998), in which the total potential of the damaged system is assumed as the sum of the deformation energy and the crack surface associated fracture energy, and the real displacement field and the crack set will minimize the total energy. Its ability to simulate very complex crack patterns without additional fracture criteria or crack tracking strategies makes it suitable for analysis of computational fracture problems, such as brittle fracture (Miehe et al., 2010, Ambati et al., 2015b), dynamic fracture (Bourdin et al., 2011, Borden, 2012), ductile fracture (Miehe et al., 2015, Ambati et al., 2015a), composite fracture (Zhang et al., 2019a, Quintanas-Corominas et

al., 2019, Zhang et al., 2021). In the present study, the ITZs are simulated by layers with homogenous thickness. To ensure the fracture energy conservation of the ITZs, an effective ITZ critical energy release rate is proposed for the phase field modeling. It is known that cover cracks can provide short paths for mass transport. Hence, in the present simulation by the red arrow, the influence of damage on mass transport is achieved by modified crack direction-dependent diffusivity tensors, as shown in Fig. 1. This is followed by an iteration step to consider the mass transport and electrochemical reactions based on the current damage degree, which forms a fully coupled non-mechanical and mechanical modeling framework.

The subsequent sections of the paper are constructed as follows. Section 2 deals with the details of the fully coupled electro-chemo-mechanical corrosion model as illustrated in Fig. 1 explaining the governing equations for the mass transport, electrochemical reactions and the meso-scale phase field model of fracture. The verification of the proposed electro-chemo-mechanical corrosion model and the parametric studies are conducted in section 3 and section 4, respectively. Section 5 presents the conclusions arisen from the study.

2. The fully coupled corrosion model

2.1. Mass transport

Mass transport in concrete represents a complex process. It not only varies with the concrete properties (e.g., mixture, hydration period, porosity) and the environmental factors (e.g., temperature, humidity, chloride concentration) but also involves various physical and chemical reactions with the surrounding cement hydrates. The mass transport process contains three main mechanisms, i.e., diffusion caused by concentration difference, convection caused by pore solution flow and migration caused by potential distribution in the electrolyte. Because this study focuses on the mass transport of moisture, chloride and oxygen, and the induced corrosion, diffusion and convection are assumed to be the main mechanisms in the present modeling. Moisture transport within concrete is very important for structural durability when corrosion is considered, as it is not only a key factor influencing chloride diffusion but also a transport medium for other ions and substances. The isothermal moisture transport at the macro-scale can be described by the Fick's second law, whose accurate prediction relies on two main factors, namely, the moisture capacity and

137   the corresponding diffusivity. The moisture capacity, which is a derivative of the equilibrium

138   sorption isotherm, can be obtained either by empirical formulas (Van Genuchten, 1980, Xi et al.,

139   1994a, Baroghel-Bouny, 2007, Huang et al., 2015a) or by considering the pore structure of the

140   cement paste (Ishida et al., 2007, Maekawa, 2008). Recently, many studies have focused on

141   modeling the water-vapor sorption isotherms taking into account the pore size distribution (Ishida

142   et al., 2007, Maekawa, 2008, Ranaivomanana et al., 2011, Huang et al., 2015a, Pinson et al., 2015,

143   de Burgh et al., 2016, Jiang et al., 2019), which can theoretically consider the effects of hydration

144   degree, temperature, hysteresis, cavitation, etc. on the moisture capacity that is very complicated to

145   be experimentally measured. Then the diffusivity, which strongly depends on the diffusion

146   mechanisms, can be predicted either by a general expression that combines the trends of different

147   mechanisms occurred in the pores (Saetta et al., 1993, Xi et al., 1994b, Muthulingam and Rao, 2014),

148   or considering multi-phase (water vapor and liquid water) transport (Daian, 1988, Ishida et al., 2007,

149   Baroghel-Bouny, 2007, Maekawa, 2008, Huang et al., 2015a). Given the water content within the

150   concrete, the transport of other substances that depend on the concrete pore solution can be

151   determined. Different models have been proposed to simulate the transport of chloride ions. A

152   critical review can be referred to Shafikhani and Chidiac (2019).

153   It should be noted that for the sake of computational efficiency, relatively large ITZ thickness

154   is adopted for the mechanical analysis (discussed in Section 2.3.2). However, this treatment might

155   not apply to mass transport analysis. Hence, in the mass transport modeling the concrete is

156   considered to be composed of impermeable aggregates and homogenized matrix (containing cement

157   paste and ITZs (Xi and Bažant, 1999)) to eliminate the influence of the artificial bigger ITZ

158   thickness on mass transport. The properties of the homogenized matrix will be discussed in Section

159   3.1.

160   2.1.1.   Moisture transport in concrete

161   According to Xi et al. (1994a) the moisture transport in concrete can be described in terms of the

162   pore relative humidity h by the mass conservation equation

$$\frac{\partial \phi_w}{\partial h}\frac{\partial h}{\partial t} - \nabla \cdot (D_h \cdot \nabla h) = 0 \tag{1}$$

163   where ϕ_w is the volume fraction of the pore water (m^3 of pore water/m^3 of concrete). Based on the

164   Brunauer-Skalny-Bodor (BSB) model of adsorption isotherm, at standard temperature and pressure,

165   the relationship between the pore water content ϕ_w and the relative humidity h can be described

166   by

$$\phi_w = \frac{CkV_m h}{(1 - kh)[1 + (C - 1)kh]} \quad (2)$$

167   where C, k, V_m are model parameters. According to Xi et al. (1994a), for the hydration period $t_e >$

168   5 days and water/cement ratio $0.3 < w/c < 0.7$, the parameters can be specified as

$$V_m = \left(0.068 - \frac{0.22}{t_e}\right)(0.85 + 0.45w/c)V_{ct} \quad (3)$$

$$C = \exp\left(\frac{855}{T}\right) \quad (4)$$

$$k = \frac{(1 - 1/n_k)C - 1}{C - 1} \quad (5)$$

169   and

$$n_k = \left(2.5 + \frac{15}{t_e}\right)(0.33 + 2.2w/c)N_{ct} \quad (6)$$

170   where T is temperature (K). V_{ct} and N_{ct} are parameters related to the type of the cement.

171   For cases that $t_e \leq 5$ days, one can set $t_e = 5$ days and for $w/c \leq 0.3$ and $w/c \geq 0.7$, set

172    $w/c = 0.3$ and $w/c = 0.7$, respectively.

173   The diffusion coefficient (m²/s) of the humidity, D_h is related to temperature, hydration

174   period, and relative humidity (Saetta et al., 1993, Muthulingam and Rao, 2014) and can be described

175   as

$$D_h = D_h^{ref} f_h(T)f_h(h)f_h(t_e) \quad (7)$$

176   where D_h^{ref} is reference diffusion coefficient.

177   The modification functions in Eq. (7) can be specified as (Bažant and Najjar, 1972)

$$f_h(T) = \exp\left[\frac{U_h}{R}\left(\frac{1}{T_{ref}} - \frac{1}{T}\right)\right] \quad (8)$$

178   where U_h is the activation energy of the moisture diffusion (kJ/mol). R is the gas constant (J/mol

179   ·K). T_{ref} is the reference temperature (K) at which D_h^{ref} is measured.

$$f_h(h) = \alpha_0 + \frac{1 - \alpha_0}{1 + (1 - h)^n/(1 - h_c)^n} \quad (9)$$

180   where α_0 is the diffusivity ratio between the minimal and maximal values of D_h. h_c is a specified

181   humidity corresponding to the middle value of D_h and n is a model parameter.

$$f_h(t_e) = 0.3 + \sqrt{\frac{13}{t_e}} \tag{10}$$

182   describes the influence of hydration period on the moisture diffusion coefficient.

183   2.1.2.   Chloride transport in concrete

184   Generally, the chlorides inside concrete exist in two forms: free chloride and bound chloride. The

185   transport of free chloride ions in non-saturated concrete can be described by (Bear and Bachmat,

186   2012, Martın-Pérez et al., 2001)

$$\frac{\partial \phi_w C_{cl}}{\partial t} = \underbrace{\nabla \cdot (D_{cl} \cdot \nabla \phi_w C_{cl})}_{\text{Diffusion}} + \underbrace{\nabla \cdot (\phi_w C_{cl} D_h \cdot \nabla h)}_{\text{Convection}} - \underbrace{\frac{\partial C_{bc}}{\partial t}}_{\text{Binding}} \tag{11}$$

187   where C_{cl} and C_{bc} are the free and bound chlorides (mol/m^3), respectively and D_{cl} is the

188   diffusion coefficient

$$D_{cl} = D_{cl}^{ref} f_{cl}(T) f_{cl}(t) f_{cl}(h) \tag{12}$$

189   where D_{cl}^{ref} is the reference diffusion coefficient measured at T_{ref}. $f_{cl}(T)$, $f_{cl}(t)$ and $f_{cl}(h)$

190   are the modification functions considering the influence of temperature, aging and relative humidity.

191   The influence of temperature on the diffusion (Bažant and Najjar, 1972) can be explained by

$$f_{cl}(T) = \exp\left[\frac{U_{cl}}{R}\left(\frac{1}{T_{ref}} - \frac{1}{T}\right)\right] \tag{13}$$

192   where U_{cl} is the activation energy of the chloride diffusion process (kJ/mol).

193   The modification function considering concrete aging (Martın-Pérez et al., 2001) can be

194   explained as

$$f_{cl}(t) = \left(\frac{t_{ref}}{t}\right)^m \tag{14}$$

195   where t_{ref} is the reference time (days) at which D_{cl}^{ref} is measured. t is the actual time in days

196   and m is an aging factor.

197   The influence of the concrete pore's relative humidity on the chloride diffusion can be

198   estimated by (Saetta et al., 1993)

$$f_{cl}(h) = \left[1 + \left(\frac{1-h}{1-h_c}\right)^4\right]^{-1} \tag{15}$$

199   where h_c is the same constant as used in Eq. (9).

The chloride binding capacity of the cement hydrates was considered using Langmuir isotherm (Luping and Nilsson, 1993, Muthulingam and Rao, 2014) and can be demonstrated as

$$C_{bc} = \frac{\alpha_L C_{cl}}{1 + \beta_L C_{cl} M_{cl}} \tag{16}$$

where α_L and β_L (m^3 of pore solution/kg) are binding constants. M_{cl} is the molar mass of chloride ion (kg/mol). Therefore, the total chloride concentration in concrete can be expressed as

$$C_{cl}^{tot} = \phi_w C_{cl} + C_{bc} \tag{17}$$

2.1.3. Oxygen transport in concrete

The equation that governs the diffusion and convection mechanisms of the oxygen can be specified as (Bear and Bachmat, 2012, Ožbolt et al., 2010)

$$\frac{\partial \phi_w C_{O_2}}{\partial t} = \underbrace{\nabla \cdot \left(D_{O_2} \cdot \nabla \phi_w C_{O_2} \right)}_{\text{Diffusion}} + \underbrace{\nabla \cdot \left(\phi_w C_{O_2} D_h \cdot \nabla h \right)}_{\text{Convection}} \tag{18}$$

where C_{O_2} is the oxygen concentration in the pore solution (mol/m^3). D_{O_2} is the effective oxygen diffusion coefficient that can be given by

$$D_{O_2} = D_{O_2}^{ref}(h) f_{O_2}(T) \tag{19}$$

where $D_{O_2}^{ref}$ is the reference oxygen diffusion coefficient measured at the reference temperature. According to the experiment results under the conditions of w/c: 0.35~0.55, T: 20~40ºC, h: 0.75~0.95 conducted by Geng et al. (2006), $D_{O_2}^{ref}$ at a temperature $T_0 = 296.15K$ can be given by

$$D_{O_2}^{ref} = 8.2236 \times 10^{-9} (w/c)^{2.346} h^{-3.247} \tag{20}$$

The temperature dependency of the oxygen diffusion can be given by Arrhenius type equation as (Pour-Ghaz et al., 2009a)

$$f_{O_2}(T) = \exp\left[\frac{U_{O_2}}{R}\left(\frac{1}{T_0} - \frac{1}{T}\right)\right] \tag{21}$$

where U_{O_2} is the activation energy of the oxygen diffusion process (kJ/mol). According to (Pour-Ghaz et al., 2009a) the activation energy of the oxygen diffusion can be given in terms of the water/cement ratio as

$$U_{O_2} = -505(w/c)^2 + 484.5 w/c - 94 \tag{22}$$

2.2. Electrochemical corrosion procedure

218   2.2.1.   Corrosion current density

219   In this study, the chloride ingress into concrete is considered to be the main reason for the

220   depassivation of the steel surface. The steel surface can be divided into active and passive zones.

221   The active zone represents the areas of steel where the chloride concentration is higher than a critical

222   value C_{cl}^{crt} (0.4% wt. of cement) (Cao and Cheung, 2014, Angst et al., 2009), and the remaining

223   steel area represent the passive zone. Coupled micro- and macro-cell corrosion mechanisms are

224   considered in the entire corrosion process (Cao et al., 2013). In order words, both anodic and

225   cathodic reactions are considered in the active zone, while the passive zone only considers the

226   cathodic reaction. Based on the Butler-Volmer expression, the current density of anodic reaction

227   (iron oxidation)

$$\text{Fe} \rightarrow \text{Fe}^{2+} + 2e^{-} \tag{23}$$
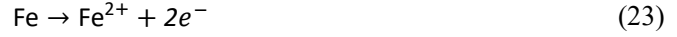
228   can be described by

$$i_{Fe} = i_{Fe}^{0} \cdot \exp\left(2.303\frac{\phi - \phi_{Fe}^{0}}{\beta_{Fe}}\right) \tag{24}$$

229   where ϕ is the electric potential (V). β_{Fe} is the anodic Tafel slope (V/dec). ϕ_{Fe}^{0} is the anodic

230   equilibrium potential. i_{Fe}^{0} is the anodic exchange current density (A/m^2). Considering the influence

231   of temperature on and the equilibrium potential the exchange density, ϕ_{Fe}^{0} and i_{Fe}^{0} can be given

232   as (Pour-Ghaz et al., 2009a, Yu et al., 2017)

$$\phi_{Fe}^{0} = \phi_{Fe}^{0,ref} + 0.000052(T - T_{ref}) \tag{25}$$

$$i_{Fe}^{0} = i_{Fe}^{0,ref} \cdot \exp\left[\frac{\alpha_{Fe} z_{Fe} F \phi_{Fe}^{0}}{R}\left(\frac{1}{T} - \frac{1}{T_{ref}}\right)\right] \tag{26}$$

233   where α_{Fe} is the symmetry factor for anodic reaction. z_{Fe} is the valency of anodic reaction. F is

234   Faraday's constant.

235   Similarly, the current density of the cathodic reaction (oxygen reduction)

$$O_2 + 2H_2O + 4e^{-} \rightarrow 4OH^{-} \tag{27}$$

236   can be described by

$$i_{O_2} = i_{O_2}^{0} \cdot \frac{C_{O_2}^{st}}{C_{O_2}^{b}} \exp\left(2.303\frac{\phi_{O_2}^{0} - \phi}{\beta_{O_2}}\right) \tag{28}$$

237   where $i_{O_2}^{0}$ is the cathodic exchange current density (A/m^2). $\phi_{O_2}^{0}$ is the cathodic equilibrium

238   potential (V). β_{O_2} is the cathodic Tafel slope (V/dec). $C_{O_2}^{st}$ and $C_{O_2}^{b}$ are the oxygen concentrations

239   at the rebar surface and concrete surface, respectively, considering the influence of oxygen

240   concentration polarization on the cathodic current density. Considering the influence of temperature

241   on and the equilibrium potential the exchange density, ϕ_{Fe}^0 and i_{Fe}^0 can be given as (Pour-Ghaz

242   et al., 2009a, Yu et al., 2017)

$$\phi_{O_2}^0 = \phi_{O_2}^{0,ref} - 0.00168\left(T - T_{ref}\right) \tag{29}$$

$$i_{O_2}^0 = i_{O_2}^{0,ref} \cdot \exp\left[\frac{\alpha_{O_2} z_{O_2} F \phi_{O_2}^0}{R}\left(\frac{1}{T} - \frac{1}{T_{ref}}\right)\right] \tag{30}$$

243   where α_{O_2} is the symmetry factor for cathodic reaction. z_{O_2} is the valency of cathodic reaction.

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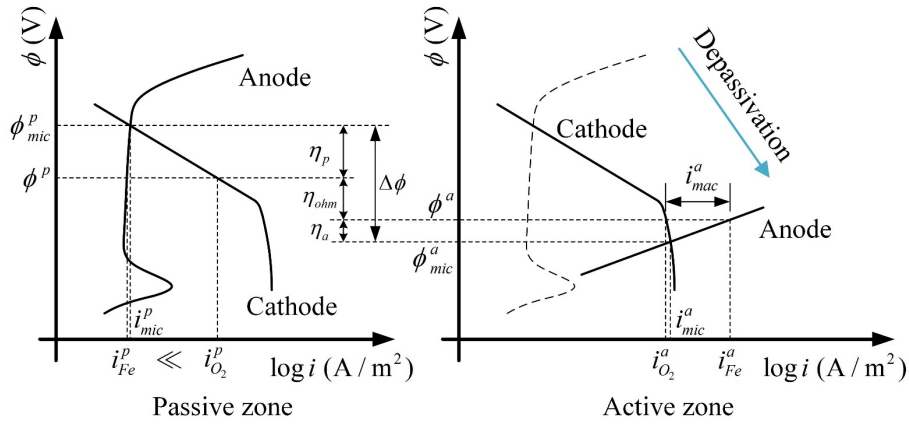
246   Fig. 2. Micro- and macro-cell polarization.

247

248   Fig. 2 shows the micro- and macro-cell corrosion mechanisms at the steel surface. In the

249   passive zone the micro-cell potential ϕ_{mic}^p and the corresponding current density i_{mic}^p can be

250   obtained by the intersection point of the anodic and the cathodic polarization curves. With the

251   increase of the chloride concentration, the anodic polarization curve moves downwards as shown in

252   Fig. 2 and the corresponding area turns into the active zone. The corresponding micro-cell potential

253   and current density are ϕ_{mic}^a and i_{mic}^a. It can be seen that the passive zone has a bigger micro-cell

254   potential ($\phi_{mic}^p > \phi_{mic}^a$), while the corresponding micro-cell current density is much smaller than

255   that of the active zone, i.e., $i_{mic}^p \ll i_{mic}^a$.

256   As shown in Fig. 2, rebar (as conductor) and concrete pore solution (as electrolyte) also form

257   a macro-cell corrosion system. The macro-cell corrosion may cause the decrease of the potential at

258   the passive zone $\eta_p = \phi_{mic}^p - \phi^p$. The corresponding anodic and cathodic current densities are i_{Fe}^p

259   and $i_{O_2}^p$. It is worth noting that i_{Fe}^p is usually much smaller than $i_{O_2}^p$, i.e., $i_{Fe}^p \ll i_{O_2}^p$, which has

$$i_{Fe}^p \cong i_{mic}^p \cong 0 \tag{31}$$

11

260   Thus, the total current density in the passive zone can be given as

$$i_{total}^p = i_{mac}^p + i_{mic}^p \cong -i_{O_2}^p \tag{32}$$

261   In the active zone the polarization may cause the increase of the potential $\eta_a = \phi^a - \phi_{mic}^a$.

262   The corresponding macro-cell anodic and cathodic current densities are i_{Fe}^a and $i_{O_2}^a$, respectively.

263   Therefore, the total macro-cell corrosion density in the active zone can be given as

$$i_{mac}^a = i_{Fe}^a - i_{O_2}^a \tag{33}$$

264   The potential difference η_{ohm} that is generated from the macro-cell corrosion current circulating

265   through concrete between the active and passive zones is termed as the ohmic drop. Accordingly,

266   the total current density (corrosion current density) in the active zone can be obtained as (Cao et al.,

267   2013)

$$i_{corr}^a = i_{mac}^a + i_{mic}^a \cong i_{Fe}^a \tag{34}$$

268   2.2.2.   Electrical potential distribution

269   The porous concrete with pore solution can be regarded as a conductor. Based on Ohm's law, a

270   Laplace equation can be adopted to describe the electrical potential distribution in the concrete

271   (Ožbolt et al., 2011, Cao et al., 2013)

$$\nabla \cdot \left(\frac{1}{\rho} \nabla \phi \right) = 0 \tag{35}$$

272   where ϕ is the electrical potential (V). ρ is the effective resistivity ($\Omega \cdot m$). Accordingly, the

273   current flux can be specified as

$$i = -\frac{1}{\rho} \nabla \phi \tag{36}$$

274   The temperature dependency of the resistivity can be given by (Pour-Ghaz et al., 2009b)

$$\rho = \rho_{ref} \cdot \exp \left[\frac{U_\rho}{R} \left(\frac{1}{T} - \frac{1}{T_{ref}} \right) \right] \tag{37}$$

275   where U_ρ is the activation energy (kJ/mol), which can be given by (Pour-Ghaz et al., 2009b)

$$U_\rho = \frac{26.753349}{1 - 4.3362256 \times \exp(-5.2488563 \cdot h)} \tag{38}$$

276   ρ_{ref} is the reference resistivity. In the present study, the electrical conductivity, which is $1/\rho_{ref}$

277   ($\Omega^{-1} \cdot m^{-1}$), is adopted (Ožbolt et al., 2011). The electrical conductivities for $w/c = 0.4$ and

278      $w/c = 0.7$ are given in Tab. 1. A linear interpolation is used to calculate the values corresponding

279   to the water/cement ratios between 0.4 and 0.7.

281 Tab. 1. Electric conductivity of concrete with different degrees of saturation(Ožbolt et al., 2011).

Saturation (%)	35	40	45	50	55	60	65	70	75	80	85	90	95
$w/c = 0.4$ (10^{-3})	0.01	0.03	0.07	0.20	0.25	0.53	0.75	1.0	2.0	6.0	10.0	11.2	12.5
$w/c = 0.7$ (10^{-3})	0.50	1.00	1.81	2.75	3.00	4.28	8.70	9.52	10.5	11.5	12.5	13.5	14.2

282

283   In electromechanical analysis, the current densities at the electrode surface can serve as

284 boundary conditions of the Laplace equation (Eq. (35)). Hence, the total flux passing through the

285 electrolyte (concrete) should be equal to the macro-cell current density at the steel surface, which is

$$i_{mac} = -\boldsymbol{n} \cdot \left(\frac{1}{\rho}\nabla\phi\right)\Big|_{\text{steel surface}} \tag{39}$$

286 where $\boldsymbol{n}$ is the unit vector normal to the rebar surface. According to Eqs. (31)-(33), the above

287 boundary condition can be rewritten as

$$i_{Fe}^a - i_{O_2}^a = -\boldsymbol{n} \cdot \left(\frac{1}{\rho}\nabla\phi\right), \quad \text{in active zone} \tag{40}$$

$$-i_{O_2}^p = -\boldsymbol{n} \cdot \left(\frac{1}{\rho}\nabla\phi\right), \quad \text{in passive zone} \tag{41}$$

288 To numerically describe the propagation of the active zone, a modified anodic Tafel slope is adopted

289 as

$$\beta_{Fe} = \begin{cases} \beta_{Fe} & \text{active zone where } \phi_w C_{cl} \geq C_{cl}^{crt} \\ \infty & \text{passive zone where } \phi_w C_{cl} < C_{cl}^{crt} \end{cases} \tag{42}$$

290 2.2.3. Oxygen consumption

291 During the electrochemical corrosion process, the cathodic reaction occurs in active and passive

292 zones. In this study, the cathodic reaction is assumed to be the only mechanism that consumes

293 oxygen. Therefore, according to Faraday's law, the relationship between the oxygen flux and the

294 cathodic current density at the steel surface can be given by

$$i_{O_2} = -z_{O_2}F \cdot \boldsymbol{J}_{O_2}, \quad \text{at steel surface} \tag{43}$$

295 where $z_{O_2} = 4$ is the valency of the cathodic reaction. F is Faraday's constant. $\boldsymbol{J}_{O_2}$ is the oxygen

296 flux. According to Fick's law, $\boldsymbol{J}_{O_2}$ can be specified as

$$\boldsymbol{J}_{O_2} = -\boldsymbol{n} \cdot D_{O_2}\nabla C_{O_2}^{st}, \quad \text{at steel surface} \tag{44}$$

297 2.2.4. Iron dissolution and rust generation

298 The corrosion of the steel bar in the concrete is a long-term process. The dissolution of the steel bar

299 is caused by the anodic reaction. According to Faraday's law, the corrosion depth of the steel surface

300 can be described by the corrosion current density as (Cao et al., 2013)

$$\frac{\partial p(\boldsymbol{x},t)}{\partial t} = \frac{M_{Fe}}{z_{Fe}F\rho_{Fe}} i_{corr}^a(\boldsymbol{x},t), \qquad \text{at active zone} \tag{45}$$

301 where $p(\boldsymbol{x},t)$ is the corrosion depth of the steel surface. M_{Fe} is the molar mass of iron. z_{Fe} is

302 the valency of anodic reaction. ρ_{Fe} is the density of the rebar.

303 As the reaction process, the rust product will form and accumulate around the steel surface.

304 The density of the insoluble rust product is larger than that of the iron. Therefore, the rust-steel

305 system will expand in volume. The volume expansion along the rebar radius direction (Suda et al.,

306 1993, Cao et al., 2013) can be given by

$$u_{rust}(\boldsymbol{x},t) = (r_v - 1) \cdot p(\boldsymbol{x},t), \qquad \text{at active zone} \tag{46}$$

307 where r_v is the volumetric expansion ratio.

308 2.3. Meso-scale Phase field model for corrosion-induced fracture

309 2.3.1. Phase field model

310 Based on (Francfort and Marigo, 1998) the potential energy of the system can be given by

$$\mathfrak{E} = \mathfrak{E}_e + \mathfrak{E}_f - \mathfrak{E}_{ext}, \qquad \text{in } \Omega \tag{47}$$

311 where $\Omega \subset \mathbb{R}^3$ is the considered domain. $\mathfrak{E}_e$ is the deformation energy, which can be specified by

$$\mathfrak{E}_e = \int_\Omega \omega_d(d) \cdot \psi_e(\boldsymbol{\epsilon}) \, dV, \qquad \text{in } \Omega \tag{48}$$

312 where $\boldsymbol{\epsilon}$ is the strain tensor and $\psi_e(\boldsymbol{\epsilon})$ is the corresponding deformation energy density. $d(\boldsymbol{x})$ is

313 the phase field value at point $\boldsymbol{x}$, in which $d = 0$ and $d = 1$ represent intact and totally damaged

314 material states. $\omega_d(d)$ is the degradation function characterizing the damage degree of the material.

315 In this study, the parametric degradation function proposed by Wu (2017) is adopted, which is

$$\omega_d(d) = \frac{(1-d)^2}{(1-d)^2 + a_1 d + a_1 a_2 d^2} \tag{49}$$

316 in which a_1 and a_2 are parameters that are related to different stress softening relationships. Here,

317 a widely adopted linear softening relationship is adopted

$$a_1 = \frac{4EG_c}{c_0 l_0 Y_t^2}, \quad \text{and} \quad a_2 = -0.5 \tag{50}$$

318 where E is the Young's modulus. Y_t is the material strength.

319 The fracture energy $\mathfrak{E}_f$ can be specified by

14

$$\mathfrak{E}_f = \int_\Omega G_c \cdot \gamma_d(d, \nabla d)\, \mathrm{d}V, \qquad \text{in } \Omega \tag{51}$$

320 where G_c is the critical energy release rate. $\gamma(d, \nabla d)$ is the crack surface density function, which

321 can be given by (Bourdin et al., 2000)

$$\gamma_d(d, \nabla d) = \frac{1}{c_0}\left[\frac{1}{l_0}\alpha(d) + l_0 \nabla d \cdot \nabla d\right] \tag{52}$$

322 where l_0 is the phase field internal length scale used to characterize the width of the smeared crack.

323 c_0 is a model parameter, which is

$$c_0 = \int_0^1 \alpha(s)\, \mathrm{d}s \tag{53}$$

324 where $\alpha(d)$ is the crack geometry function. In this study, a polynomial form (Wu, 2017) is adopted

325 as

$$\alpha(d) = 2d - d^2 \tag{54}$$

326 The external energy $\mathfrak{E}_{ext}$ can be specified by

$$\mathfrak{E}_f = \int_\Omega \bar{\boldsymbol{b}} \cdot \boldsymbol{u}\, \mathrm{d}V + \int_{\Gamma_t} \bar{\boldsymbol{t}} \cdot \boldsymbol{u}\, \mathrm{d}S \tag{55}$$

327 where $\bar{\boldsymbol{b}} \in \mathbb{R}^3$ is the body force. $\bar{\boldsymbol{t}} \in \mathbb{R}^2$ is the boundary force at $\Gamma_t \subset \mathbb{R}^2$.

328 According to the Francfort-Marigo variational principle (Francfort and Marigo, 1998), the

329 governing equations and boundary conditions can be obtained as

$$\nabla \cdot [\omega_d(d)\boldsymbol{\sigma}] + \bar{\boldsymbol{b}} = \boldsymbol{0}, \qquad \text{in } \Omega \tag{56}$$

$$\frac{G_c}{c_0 l_0}[\alpha'(d) - 2l_0\Delta d] = -\omega_d'(d)\mathcal{H}_t, \qquad \text{in } \Omega \tag{57}$$

$$\omega_d(d)\boldsymbol{\sigma} \cdot \boldsymbol{n} = \bar{\boldsymbol{t}}, \qquad \text{on } \Gamma_t \tag{58}$$

$$\nabla d \cdot \boldsymbol{n} = \boldsymbol{0}, \qquad \text{on } \Gamma \tag{59}$$

330 where $\mathcal{H}_t$ is a solution dependent variable used to prevent self-healing of the damage (Miehe et

331 al., 2010), which can be specified by

$$\mathcal{H}_t = \max_{\tau \in [0,t]}\{\psi_e(\boldsymbol{\epsilon}, \tau)\} \tag{60}$$

332 2.3.2.   Meso-scale phase field model

333 Concrete is a multi-phase material containing aggregates, mortar and the ITZs between them.

334 Generally, the computational fracture modeling of concrete is usually conducted in two length scales:

335 computational mechanics (macro-scale) and computational mesomechanics (meso-scale). In macro-

336 scale modeling, concrete is treated as a homogenous material, with effective material properties

15

337   obtained from experimental tests or numerical homogenization methods. The heterogeneity of the

338   concrete is not considered at this scale, so it is very suitable for large-scale modellings. However,

339   for corrosion-induced fracture the damage usually occurs within the concrete cover, whose thickness

340   is usually 10mm $-$ 50mm and is comparable to the diameter of the coarse aggregate (usually

341   2.4mm $-$ 19.05mm). The heterogeneity of the concrete cover due to the presence of aggregates will

342   have significant influences on both the damage and mass transport processes. Therefore, in this

343   study, a meso-scale model, which can explicitly consider different phases, is adopted to simulate the

344   entire corrosion process of the reinforced concrete accurately.

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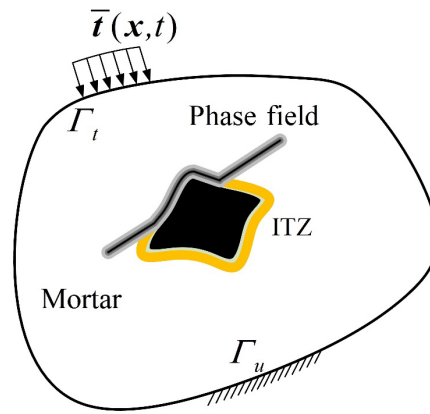
346
347   Fig. 3 Meso-scale phase field model for concrete cracking.

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349   Fig. 3 shows the meso-scale phase field model for concrete cracking. In the model, the mortar,

350   the aggregate and the ITZs are regarded as homogenous isotropic materials. Accurate modeling of

351   the ITZ damage poses a challenge because of the complex topology and extremely thin thickness

352   (usually tens of micrometers). However, recent investigations show that in the fracture modeling,

353   an approximate ITZ thickness of 0.1mm $-$ 1mm can be adopted to characterize the damage

354   behavior in the meso-scale model and will not significantly affect the fracture behavior of the

355   structure (Šavija et al., 2013, Du et al., 2014, Huang et al., 2015b, Zhou et al., 2017, Zhang et al.,

356   2019b, Hu et al., 2022). In the present study, the ITZ thickness is assumed to be 0.5mm based on

357   previous studies (Hu et al., 2022). Then the ITZ damage and mortar cracking are characterized using

358   a unified phase field modeling framework. To further reduce the computational effort, we assume

359   that the smeared crack width can be wider than the ITZ. Then, an effective ITZ critical energy

360   release rate $\tilde{G}_i$ is proposed to prevent the non-conversation of the ITZ fracture energy that is caused

361 by the inconsistency between the smeared crack width and ITZ thickness. According to the fracture

362 energy conservation $\tilde{G}_i$ can be obtained by

$$G_i = \int_0^{l_z} \tilde{G}_i \cdot \gamma_d(d, \nabla d)\, \mathrm{d}x + \int_{l_z}^{D_c} G_m \cdot \gamma_d(d, \nabla d)\, \mathrm{d}x \qquad (61)$$

363 where G_i and G_m are the critical energy release rates of the ITZ and the mortar, respectively. l_z

364 is the thickness of the ITZ. D_c is the half width of the smeared crack and d is the phase field

365 distribution along the ITZ thickness direction. According to the analytical solution of the 1-D phase

366 field model, D_c and d can be given as (Wu, 2017)

$$D_c = \frac{\pi}{2} \cdot l_0 \qquad (62)$$

$$d = 1 - \sin\left(\frac{x}{l_0}\right) \qquad (63)$$

367 Substituting Eqs. (62) and (63) into Eq. (61), the effective critical energy release rate of the ITZ can

368 be obtained as

$$\tilde{G}_i = \frac{[2G_i c_0 - G_m c_0 + G_m \sin(2l_z/l_0)]l_0 + 2G_m l_z}{\sin(2l_z/l_0)\, l_0 + 2G_m l_z} \qquad (64)$$

369 2.3.3.   Influence of damage on mass transport

370 In the past few decades, considerable work has been done to investigate the influence of concrete

371 damage on the mass transport process. Experimental observations show that surface cracks increase

372 the ingress of different substances into concrete (Aldea et al., 2000, Wang et al., 1997). Based on

373 the results, Ožbolt et al. (2010) tried to propose the moisture diffusion coefficient of the damaged

374 region using the undamaged diffusion coefficient multiplied by a normalized permeability

375 coefficient and validated it as shown in Fig. 4. This modified moisture diffusion coefficient is

376 adopted in the present study and is represented as

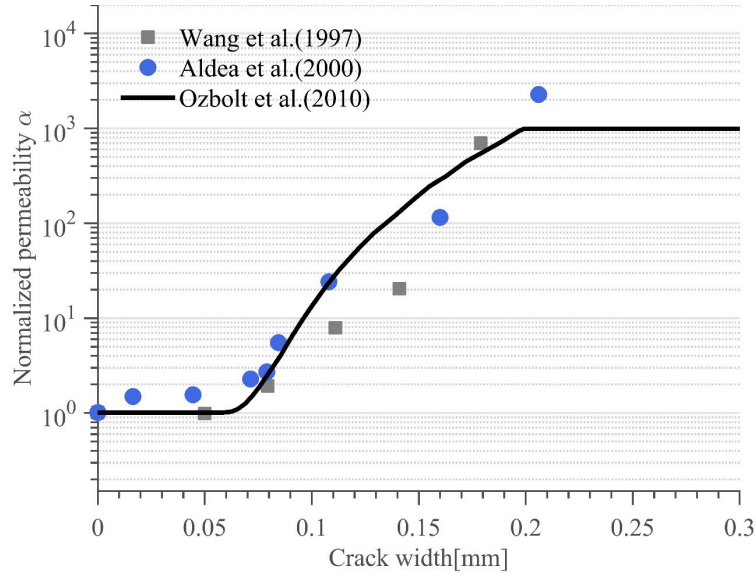$$D_h^c = \alpha \cdot D_h \qquad (65)$$

377

Fig. 4. The relationship between the crack width and the normalized permeability.

For oxygen diffusion, the coefficient can be drastically increased with the increasing of the crack width. According to Cao et al. (2013), the flow of oxygen through cracks can be described by Poiseuille's law for laminar flow. Therefore, the oxygen diffusion coefficient within cracks can be given by

$$D_{O_2}^c = D_{O_2} \cdot \left(\frac{[\![u]\!]}{[\![u]\!]_c} \right)^3, \quad \text{for } [\![u]\!] > [\![u]\!]_c \qquad (66)$$

where $[\![u]\!]$ is the crack width. $[\![u]\!]_c$ is a critical crack width beyond which the effect of damage on diffusivity should be considered.

Djerbi et al. (2008) investigated the effect of transverse crack on the chloride diffusion. Based on the experimental results, they found that the crack width has a significant influence on the chloride diffusivity, which can be given by

$$D_{cl}^c = \begin{cases} 2 \times 10^{-11} [\![u]\!] - 4 \times 10^{-10}, & \text{for } 30\mu m \leq [\![u]\!] \leq 80\mu m \\ 14 \times 10^{-10}, & \text{for } [\![u]\!] > 80\mu m \end{cases} \qquad (67)$$

Modified diffusion coefficients in Eqs. (65)-(67) show that the diffusivity is highly related to the crack width. Theoretically, the modified diffusion coefficient within the cracks should be explicitly considered in the modeling with the moving crack surfaces as boundary conditions. However, even for very simple crack patterns, it will be a very complicated task. Therefore, in the present study, the modified coefficients are implicitly considered by using an effective crack width specified by

$$[\![u]\!]_{eff} = \langle \epsilon_1 \rangle_+ \cdot \omega_d(d) h_e \qquad (68)$$

18

396   where the bracket operator is defined as

$$\langle \epsilon_1 \rangle_+ = \frac{\epsilon_1 + |\epsilon_1|}{2} \tag{69}$$

397   in which ϵ_1 is the first principal strain. h_e is the characteristic element length. However, the

398   effective crack width in Eq. (68) cannot be directly used in Eqs. (65)-(67). Because the increase of

399   the diffusion coefficient only occurs within the cracks. Direct utilization of Eq. (68) will implement

400   a modified diffusivity to the whole element, which will cause a significant element size sensitivity

401   and inconsistency with the experimental observations. Therefore, to correctly consider the modified

402   diffusivity, we assume that the diffusion coefficient in the damaged elements consists of two parts:

403   the coefficient of the intact concrete and the increased coefficient due to damage. Thus, the modified

404   diffusion coefficient can be given by

$$\widetilde{D}_X^c = D_X + \Delta D_X^c \tag{70}$$

405   where X represents the considered substances, i.e., moisture, chloride and oxygen. ΔD_X^c is the

406   increased coefficient attributed to the damage, which is given by

$$\Delta D_X^c = \frac{D_X^c\big([\![u]\!]_{eff}\big) \cdot [\![u]\!]_{eff}}{h_e} = D_X^c\big([\![u]\!]_{eff}\big) \cdot \omega_d(d)\langle \epsilon_1 \rangle_+ \tag{71}$$

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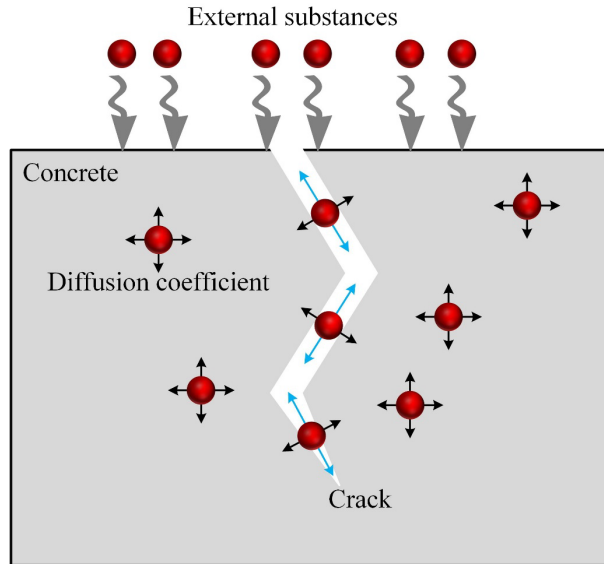
Fig. 5. Substance diffusion coefficient in cracked concrete.

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411   Fig. 5 illustrates the transport process of the substances within cracked concrete. External

412   substances and the diffusion coefficient are denoted by the red balls and the attached arrows. The

413   figure shows that the diffusion coefficient is isotropic in the intact zone. However, the diffusion

19

414 coefficient becomes anisotropic for substances transported through cracks. For direction along the

415 crack surface, the coefficient is significantly increased, which is described by Eq. (71). For direction

416 perpendicular to the crack surface, the coefficient remains the same as that in the intact zones. Hence,

417 to achieve this crack direction dependent diffusion coefficient, we propose an anisotropic coefficient

418 tensor as

$$\widetilde{\boldsymbol{D}}_X^c = D_X \cdot \boldsymbol{I} + \Delta D_X^c \cdot (\boldsymbol{I} - \boldsymbol{n_1} \otimes \boldsymbol{n_1}) \tag{72}$$

419 where $\boldsymbol{I}$ is the second-order unit tensor. $\boldsymbol{n_1}$ is the unit vector perpendicular to the crack surface,

420 which can be specified by

$$\boldsymbol{n_1} = \frac{\nabla d}{\|\nabla d\|} \tag{73}$$

421 In order to clearly demonstrate the influence of Eq. (72) on the diffusion process, we consider

422 a simple steady state of substance X diffusion, whose governing equation can be specified by

$$\nabla \cdot (D_X \nabla C_X) = 0 \tag{74}$$

423 in which D_X is the isotropic diffusion coefficient. Assuming a zero-flux boundary condition W_X,

424 Eq. (74) can be considered as a Euler equation of the following variational principle

$$C_X = \text{Arg} \left\{ \inf_{W_X} I_X(C_X) \right\} \tag{75}$$

425 in which $I_X(C_X)$ is a kind of generalized free energy of diffusion. One of the possible forms of

426 $I_X(C_X)$ that satisfies Eqs. (74) and (75) can be given by

$$I_X(C_X) = \frac{1}{2} \int_\Omega D_X \cdot \|\nabla C_X\|^2 \, \mathrm{d}V \tag{76}$$

427 According to Eqs. (72) and (76), the generalized free energy of diffusion at the damaged zone

428 can be given by

$$I_X^c(C_X) = \frac{1}{2} \int_\Omega \widetilde{\boldsymbol{D}}_X^c : \nabla C_X \otimes \nabla C_X \, \mathrm{d}V \tag{77}$$

429 Substituting Eq. (72) into Eq. (77), it has

$$I_X^c(C_X) = \frac{1}{2} \int_\Omega \left[D_X + \Delta D_X^c \cdot \sin^2\langle \boldsymbol{n_1}, \nabla C_X \rangle \right] \cdot \|\nabla C_X\|^2 \, \mathrm{d}V \tag{78}$$

430 By mimicking Eq. (76), an effective diffusion coefficient at the cracked zone can be given as

$$D_X^{eff} = D_X + \Delta D_X^c \cdot \sin^2\langle \boldsymbol{n_1}, \nabla C_X \rangle \tag{79}$$

431 Through the above derivations, it can be seen that Eq. (79) is actually equivalent to Eq. (72).

432 Let θ denote the angle between the crack direction and the gradient of concentration of X. The

433 relationship between the effective diffusion coefficient and θ is depicted in Fig. 6. In the figure,

20

434   lines with different colors represent different damage degrees, i.e., crack widths. It can be seen that

435   for the intact zones ($\omega_d = 1$) the diffusion coefficient is isotropic and equal to D_X. For the damaged

436   zones, the coefficients along and perpendicular to the crack direction are increased and unchanged,

437   respectively. In addition, the diffusion coefficient along the crack direction increases with the

438   increase in the crack width, which is consistent with the experimental observations (Djerbi et al.,

439   2008).

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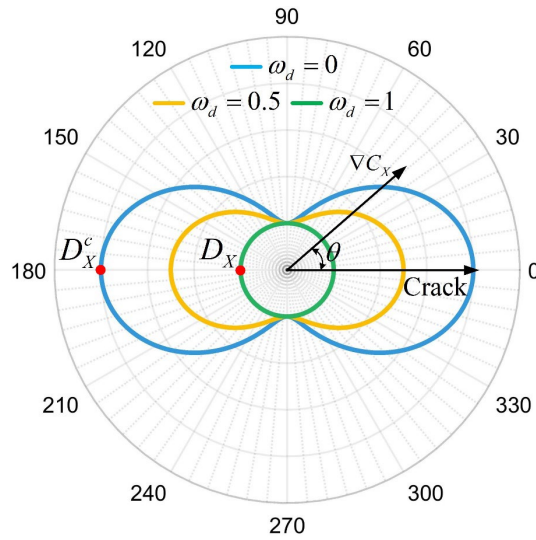
441
442   Fig. 6. Crack direction dependent diffusion coefficient.

3. Verification

3.1. Specimen and material properties

The proposed meso-scale electro-chemo-mechanical model was verified by an experiment

conducted by Ye et al. (2017). The geometry and boundary conditions of the experiment program

are shown in Fig. 7. Four rebars of diameter *12* mm are embedded in the corners of the specimen

and denoted as C10, C15, C20 and C25 based on their distances from the concrete surfaces. The

specimens were placed in an environmental chamber with 33°C and *80%* relative humidity. The

surface chloride concentration $C_{cl}^s(t) = 0.12t^{0.54}$ suggested by (Muthulingam and Rao, 2014) is

adopted. The oxygen concentration at the concrete surface is assumed to be *0.268* mol/m^3 (Cao et

al., 2013). The material properties for mass transport used by Muthulingam and Rao (2014) and

Ožbolt et al. (2010) shown in Tab. 2 are adopted. The electrochemical properties for corrosion used

by Cao et al. (2013) and Zhu and Zi (2017) are adopted as given in Tab. 3.
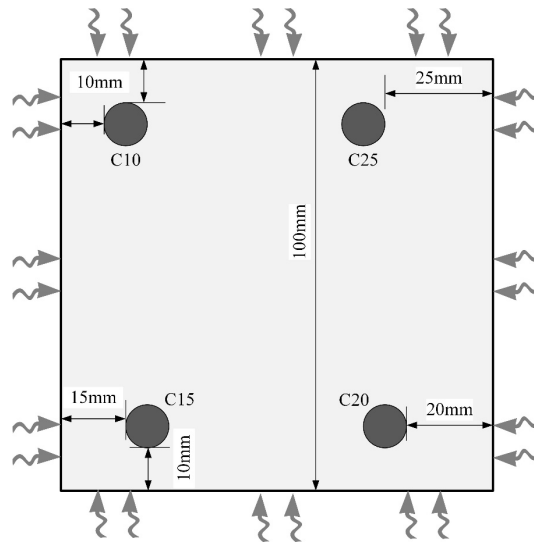
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Fig. 7. Geometry of the specimen and rebars.

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459   Tab. 2. Properties for mass transport. (Muthulingam and Rao, 2014, Ožbolt et al., 2010)

property	value
Reference moisture diffusion coefficient D_h^{ref}	2×10^{-11} m²/s
Moisture diffusion activation energy U_h	20.3 kJ/mol
Gas constant R	8.31 J/mol
Reference temperature T_{ref}	296 K
Specified relative humidity h_c	0.75
Moisture diffusivity ratio α_0	0.05
Model parameter for humidity n	10
Hydration period t_e	28 days
Water/cement ratio w/c	0.5
Reference chloride diffusion coefficient D_{cl}^{ref}	3.4×10^{-12} m²/s
Binding constant α_L	0.39
Binding constant β_L	0.07 m³/kg
Molar mass of chloride ion M_{cl}	35.5 g/mol
Chloride diffusion activation energy U_{cl}	44.6 kJ/mol
Reference time t_{ref}	28 days
Aging factor m	0.15

460

461   Tab. 3. Properties for electrochemical corrosion. (Cao et al., 2013, Zhu and Zi, 2017)

Property	Value
Anodic exchange current i_{Fe}^0	3×10^{-4} A/m²
Cathodic exchange current $i_{O_2}^0$	1×10^{-5} A/m²
Anodic equilibrium potential ϕ_{Fe}^0	-0.78 V
Cathodic equilibrium potential $\phi_{O_2}^0$	0.16 V
Anodic Tafel slope β_{Fe}	0.09 V/dec

Cathodic Tafel slope β_{O_2}	0.18 V/dec
Faraday's constant F	96486.7
Volumetric expansion ratio r_v	2.96
Molar mass of iron M_{Fe}	55.845 g/mol
Density of rebar ρ_{Fe}	7.87 g/cm^3

462

463   For normal strength concrete, the Young's modulus of the coarse aggregate can be estimated

464   according to the Code (2005) as

$$E_a = 22\left(\frac{f_a}{10}\right)^{0.3} \tag{80}$$

465   where f_a is the corresponding cubic compressive strength. According to (Contrafatto et al., 2016,

466   Li et al., 2021), f_a can be set to be 122.63 MPa.

467   According to Lu et al. (2005) the Young's modulus of the homogenized concrete E_c can be

468   estimated by

$$E_c = \frac{100}{2.2 + 34.74/f_c} \tag{81}$$

469   where f_c is the cubic compressive strength of the concrete. In the experiment, this parameter was

470   measured by Ye et al. (2017) as $f_c = 42.5$ MPa. Then, by using the Mori-Tanaka homogenization

471   theory (Mori and Tanaka, 1973, Li et al., 2021), the Young's modulus of the mortar E_m can be

472   estimated by

$$E_c = E_m + \frac{V_a(E_a - E_m)}{1 + (1 - V_a)g_m} \tag{82}$$

473   in which V_a is the aggregate volume fraction. In the present study, a place and take aggregate

474   generation algorithm (Xi et al., 2018b) is adopted, and a volume fraction about 0.37~0.4 is adopted

475   for all the simulations. g_m is a parameter, which can be specified by

$$g_m = \frac{E_a - E_m}{E_m + 4\mu_m/3} \tag{83}$$

476   where

$$\mu_m = \frac{E_m}{2(1 + v_m)} \tag{84}$$

477   where v_m is the Poisson's ratio of the mortar. In the present study, the Poisson's ratio 0.2 is used

478   for the homogenized concrete, the mortar and the aggregate (Huang et al., 2016, Li et al., 2021).

479   The corrosion-induced fracture is modeled by the meso-scale phase field model introduced in

480   section 2.3. As the model explicitly considers different phases, the corresponding fracture properties

23

481 such as material strength and critical energy release rate, are used in the analysis. According to Nagai

482 et al. (2005), the tensile strength Y_m and the tensile critical energy release rate G_m of the mortar

483 can be estimated by

$$Y_m = 1.4 \cdot \ln\left(f_m^{'}\right) - 1.5 \tag{85}$$

$$G_m = (0.0469d_a^2 - 0.5d_a + 26)\left(\frac{f_m^{'}}{10}\right)^{0.7} \tag{86}$$

484 where the parameter $d_a = 2.36$mm (Li et al., 2021). $f_m^{'}$ is the cylinder compressive strength of

485 the mortar that can be estimated by (Sideris et al., 2004)

$$f_m^{'} = \frac{E_m - 12.4147}{0.2964} \tag{87}$$

486 For ITZ damage, the tensile strength Y_i can be estimated by (Nagai et al., 2005)

$$Y_i = -1.44C_w + 2.3 \tag{88}$$

487 where

$$C_w = \frac{1}{0.047f_m^{'} + 0.5} \tag{89}$$

488 Finally, based on previous studies (López et al., 2008, Huang et al., 2016), the ITZ tensile critical

489 energy release rate is set to be half that of the mortar, i.e., $G_i = 0.5G_m$.

490 According to Xi and Bažant (1999) when considering aggregate volume fraction less than 50%,

491 the matrix can be assumed to be composed of bulk cement past and ITZs, and the properties of the

492 matrix should be considered as a function of the aggregate content. As suggested by Xi and Bažant

493 (1999) the relationship between the diffusivities of the concrete D_c and the matrix (i.e., cement

494 paste and ITZs) D_m can be expressed as (Christensen, 1979)

$$D_c = D_m \frac{2(1 - V_a)}{2 + V_a} \tag{90}$$

495 In the present simulation, this equation is used to evaluate the diffusion coefficient of the matrix

496 (i.e., mortar and ITZs). It is because that for mechanical analysis, relatively large ITZ thickness is

497 adopted to reduce the computation efforts as discussed in Section 2.3.2. However, this strategy

498 might not apply to diffusion analysis. Eq. (90) treating cement paste and ITZs as a homogenized

499 matrix, makes it possible for the present simulation to adopt a larger ITZ thickness as well as

500 consider the influence of the ITZs on the diffusivity in a more reasonable way. This equation is used

501 for all the substances considered in the mass transport process.

3.2. Results

As non-uniform rust expands at the rebar surfaces, the predicted crack patterns are depicted in Fig. 8. It can be seen that all cracks are concentrated near the rebars, and the cracks tend to develop along the ITZs, which are the weakest regions in the concrete domain. The coarse aggregates near the surface significantly affect the surface's crack position and propagation. This can be attributed to the comparable sizes of the coarse aggregates and the concrete cover thickness. In summary, the surface crack tends to initiate near bigger aggregates, then propagates along the ITZs and the mortar between them, creating an additional path for mass transport, which will surely increase the corrosion process. The corner spalling phenomenon observed in the experiment conducted by Fischer (2012) is accurately predicted by the present simulation, as shown in Fig. 8. It can be seen that corner rebars, equidistant from the upper and the left concrete surfaces, form a scissors-like crack pattern: two cracks perpendicular to the surfaces and two inline cracks inclined to the surfaces. Additionally, it can be observed that the cracks between two rebars tend to merge leading to concrete cover delamination.
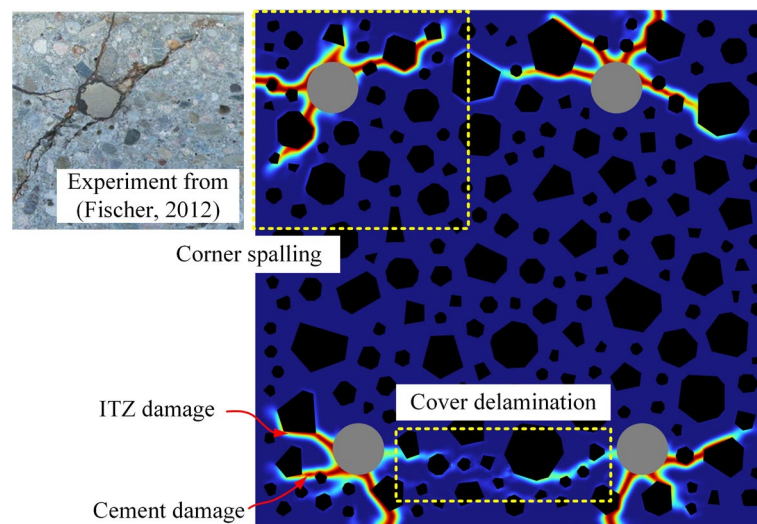
Fig. 8. Predicted crack patterns and comparison with the experimental corner spalling.

Fig. 9 shows the relationships between the steel loss ratio, defined as the ratio between the loss cross-sectional area of the rebar and the original area, and the surface crack width for different rebar locations. These are compared with the experimental results from Ye et al. (2017). It is noteworthy that the experiment was conducted in an accelerated timeframe, so in this section, only the steel loss

25

524 ratio is considered instead of the corrosion time. Fig. 9 shows that for all four rebars, the surface

525 crack widths increase with the corrosion propagation, and the predicted results agree well with the

526 experimental observations. In addition, the steel loss ratio versus crack width curves for C15, C20

527 and C25 show clear jumps at different steel loss ratios. This is caused by the sudden damage of the

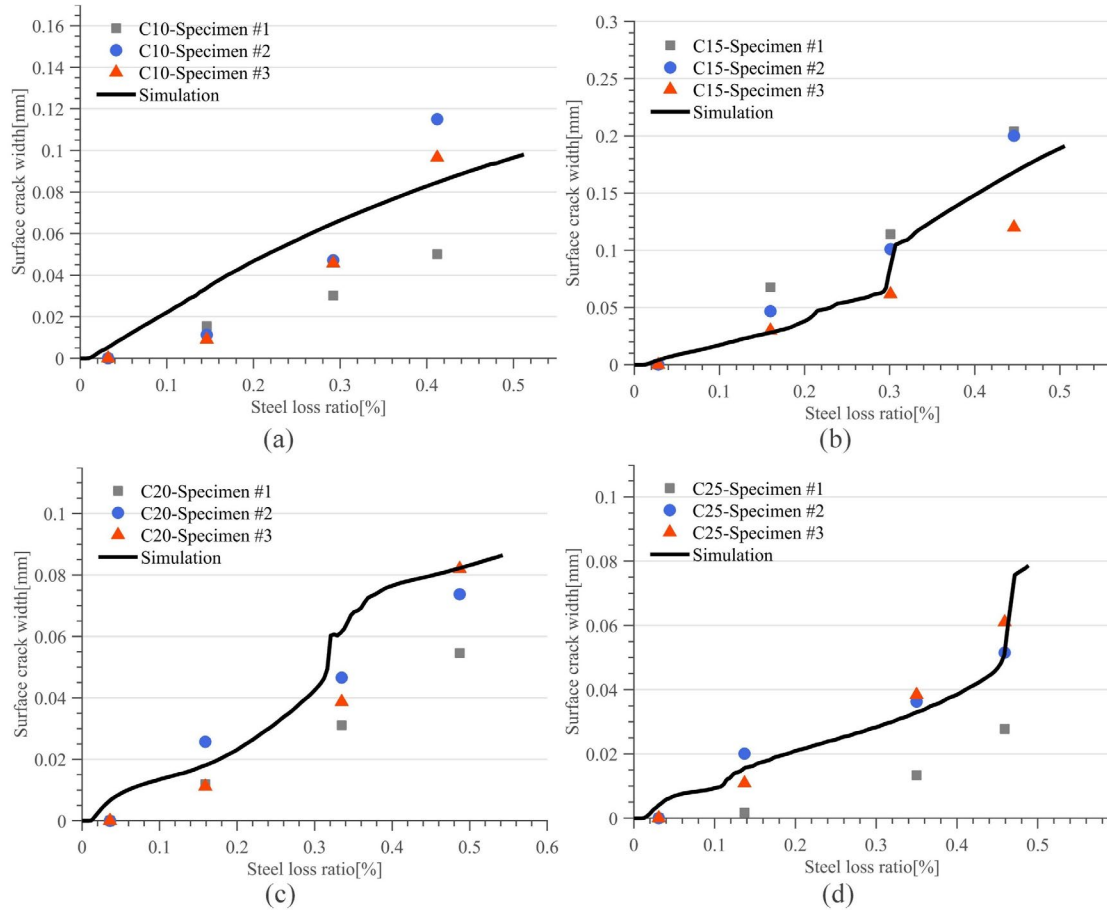528 surface cracks, especially when relatively large aggregates exist near the concrete surface.

529

Fig. 9. Predicted and experimental results of the steel loss ration versus surface crack width at different locations: (a) C10; (b) C15; (c) C20; (d) C25.

4. Parametric studies

535 To investigate the influences of variations in aggregate distribution, cover thickness, humidity and

536 temperature on the entire corrosion process, a 2-D RC beam with one rebar at the center is

537 considered. The dimensions of the beam and placement of the rebar (12mm diameter) are depicted

538 in Fig. 10. The meso-scale model is explicitly considered for only the top section of the beam, with

539   aggregates, mortar and the ITZs to reduce the computational cost. Other regions are simulated by

540   using a homogenized model. In all the following simulations, a phase field internal length scale

541    $l_0 = 1.0$mm is adopted. Theoretically, an accurate way to assess the serviceability of a RC structure

542   would be to model its loading capacity during corrosion. However, due to the high computational

543   effort, the present study adopted a surface crack width of 0.3mm as the serviceability assessment

544   criterion as suggested by (Hu et al., 2022).

545

546
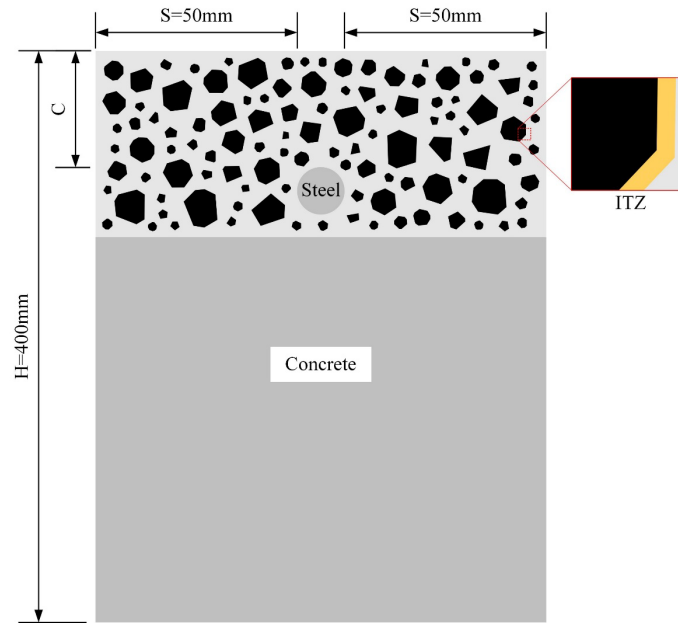
547   Fig. 10. Meso-scale model of the RC beam with one rebar.

548

549   4.1. Influence of aggregate distribution on the corrosion-induced fracture

550   In order to investigate the influence of the aggregate distribution, 10 random meso-scale models are

551   considered for the entire corrosion process simulation. The concrete cover thickness is $C = 30$mm.

552   As suggested by Muthulingam and Rao (2014), the chloride concentration at the concrete surface is

553   set to be $C_{cl}^s(t) = 0.12t^{0.54}$. The oxygen concentration dissolved in the surface pore solution is

554   assumed to be 0.268 mol/m^3 (Cao et al., 2013). The environmental temperature and humidity are

555   23°C and 70%, respectively.

556   Fig. 11 shows the predicted crack patterns of the ten random meso-scale models. The typical

557   crack patterns for different cases are quite similar, containing two side cracks and one vertical crack.

558　As shown in the figure, side cracks initiate from the rebar surface due to the tensile stress state and

559　then propagate to the lateral surfaces of the beam. On the contrary, the vertical cracks initiate from

560　the top of the beam and propagate to the rebar (Xi and Yang, 2017). It can be observed that the

561　specified paths are different and significantly affected by the aggregate locations, thus showing the

562　influence of the aggregate distribution on the crack path. The overall crack patterns of the 10 random

563　meso-scale models are summarized in Fig. 12(a) by solid red lines where the grey areas represent

564　the potential damage areas of the RC beam subjected to corrosion. It can be seen that the potential

565　cracking area agrees well with the experimental results (Amalia et al., 2018).

566

Random model 1　　　　　Random model 2

Random model 3　　　　　Random model 4

Random model 5　　　　　Random model 6

Random model 7　　　　　Random model 8

Random model 9　　　　　Random model 10
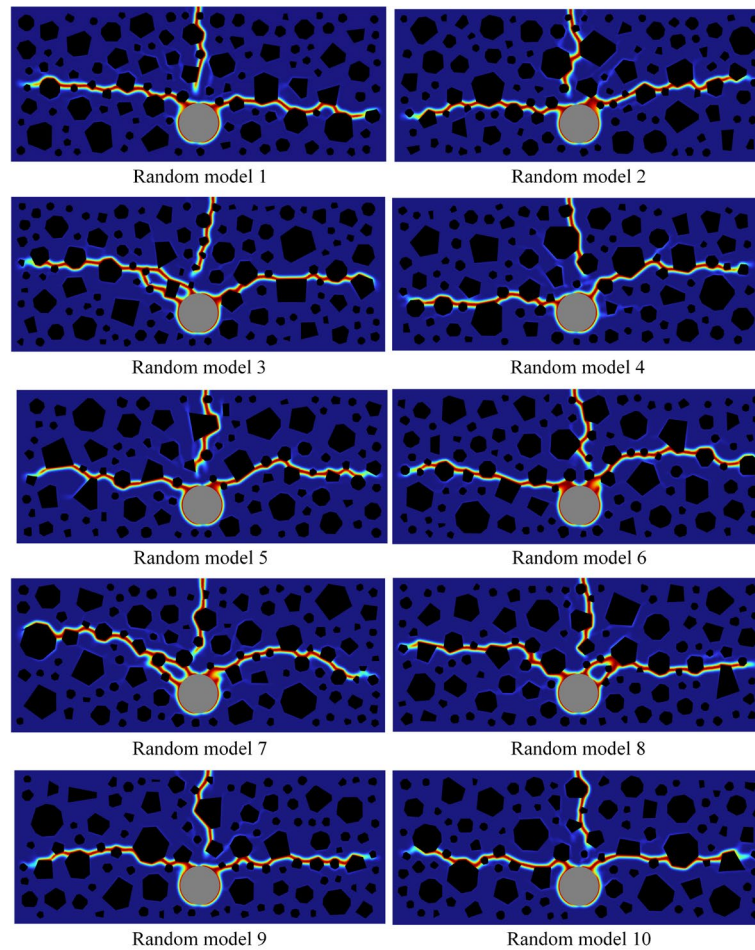
567
568　　　　Fig. 11. Crack patterns of 10 random meso-scale models at critical crack width.
569

28

(a)   (b)
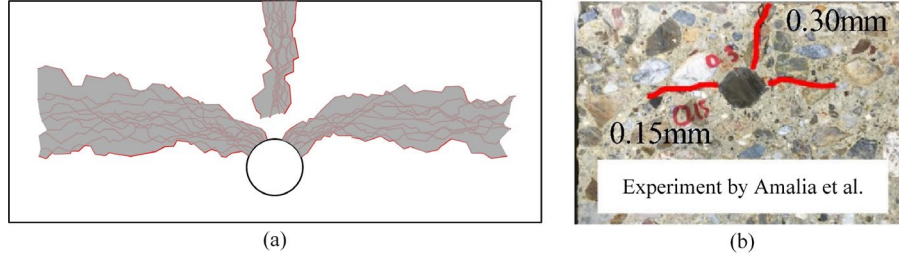
Fig. 12. Summary of crack patterns from (a) different random mesoscale models and (b) experimental data (Amalia et al., 2018).

The corrosion depth (dissolved iron) $p(\mathbf{x}, t)$ and the rust expansion $u_{rust}(\mathbf{x}, t)$ for different random models when the surface cracks reach the critical crack width are shown in Fig. 11, where both $p(\mathbf{x}, t)$ and $u_{rust}(\mathbf{x}, t)$ are scaled up by 10 times for a better illustration. It seems that the depassivation initiates first from the top surface of the rebar, resulting in localized corrosion. The corrosion propagates towards the bottom, and micro-cell corrosion dominates the corrosion process, resulting in homogenous corrosion of the entire rebar. Therefore, the ultimate corrosion shape will be like a semi-ellipse band. The figure shows that the aggregate distribution has a minor influence on the corrosion depth (represented by red areas) and the rust accumulation (represented by yellow areas). Fig. 14 shows the average corrosion densities of different aggregate distributions when the critical surface crack width is reached. It can be observed that the average corrosion densities of the 10 random models varies with the aggregate distribution, which is consistent with the shapes of the corroded rebars, as depicted in Fig. 13.
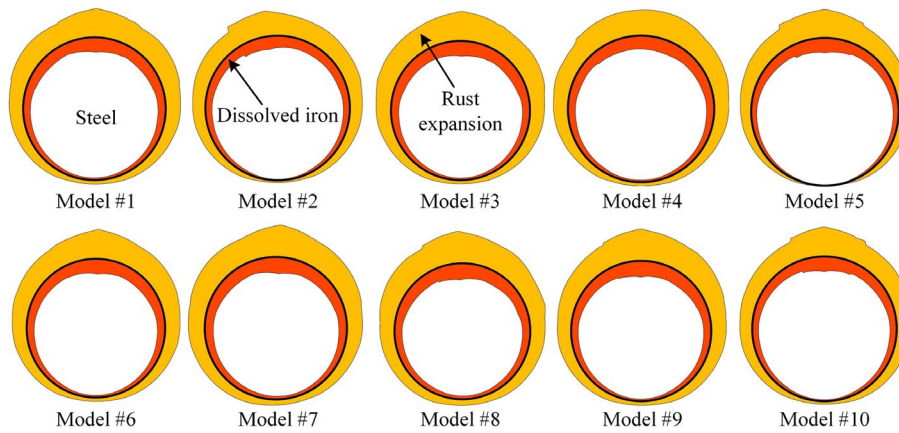

Fig. 13. Shape of corroded rebars for 10 random meso-scale models at critical crack width.
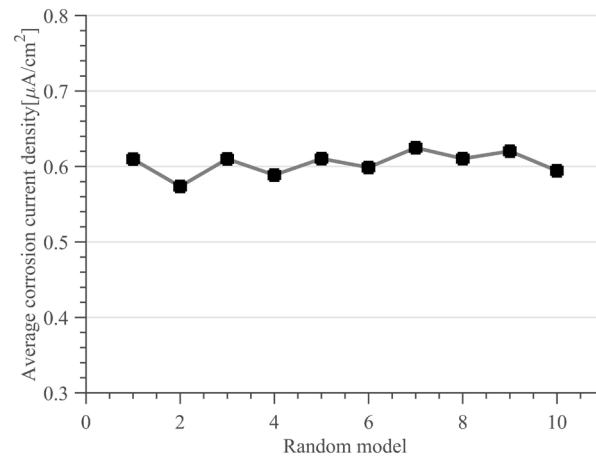(Deformation scale factor: 10)

29

Fig. 14. Average corrosion current densities for different random meso-scale models at critical crack width.

Fig. 15 shows the time-surface crack width curves of the different aggregate distributions. It can be seen that all the curves show first a rapid increase until 0.07mm $- 0.1$mm. After that, the curves become flatter, showing a nearly bilinear form. The rapid increase in the surface crack width is caused by the stress transfer within the concrete cover, and a larger cover depth will result in wider surface crack, especially when the rust accumulation is localized on the top area of the rebar. This size effect of the concrete cover will be carefully discussed in the following section. For the surface crack width curves depicted in Fig. 15, it can be seen that for different cases the surface cracks initiate between the 11.55th and 13.2th year, and reach the critical crack width 0.3 mm between 20.12th and 24.51th year. In most cases, the average time from crack initiation to reaching its critical width is about 9.94 years.
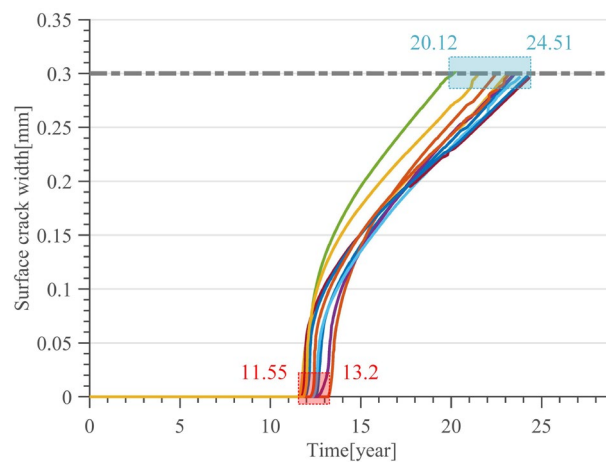

Fig. 15. Time-surface crack width curves of 10 random meso-scale models.

30

609　4.2.　Influence of cover thickness on the corrosion-induced fracture

610　In this section, three different cases, i.e., $C = 20$mm, $C = 30$mm and $C = 40$mm, are considered

611　to investigate the influence of the concrete cover thickness C on the corrosion process. The

612　aggregate distribution of the thicker cover case is constructed based on that of the thinner cover,

613　ensuring a relatively identical aggregate distribution around the rebar as shown in Fig. 16. Fig. 16

614　shows the crack patterns for different cover thicknesses, which look quite similar in terms of both

615　vertical and side cracks. However, for $C = 40$mm, Fig. 16 shows that there are two additional

616　smaller side cracks around the rebar. This may be because thicker cover thickness leads to higher

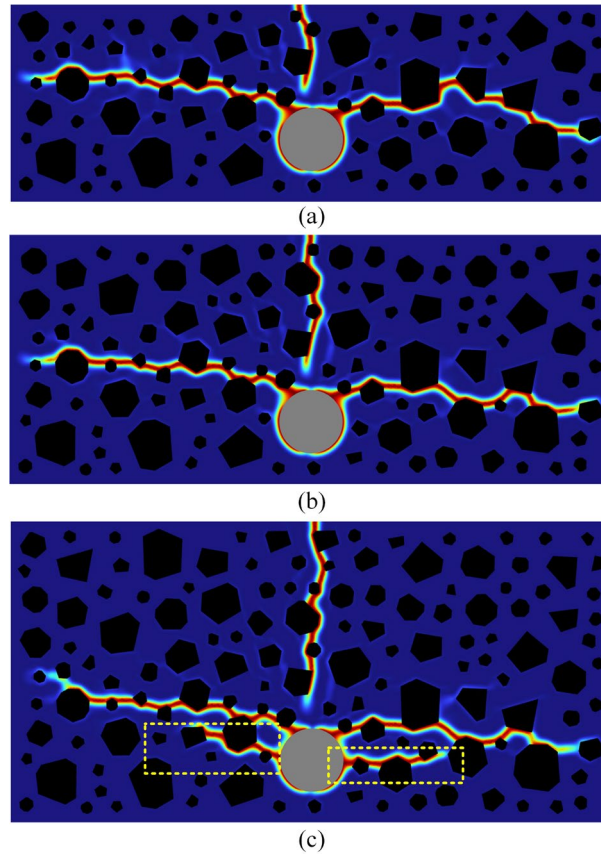617　expansive pressure, resulting in more cracks to release this constraint.

618

(a)

(b)

(c)

619

620　Fig. 16. Crack patterns for different cover thicknesses at critical surface width: (a) C=20mm; (b)
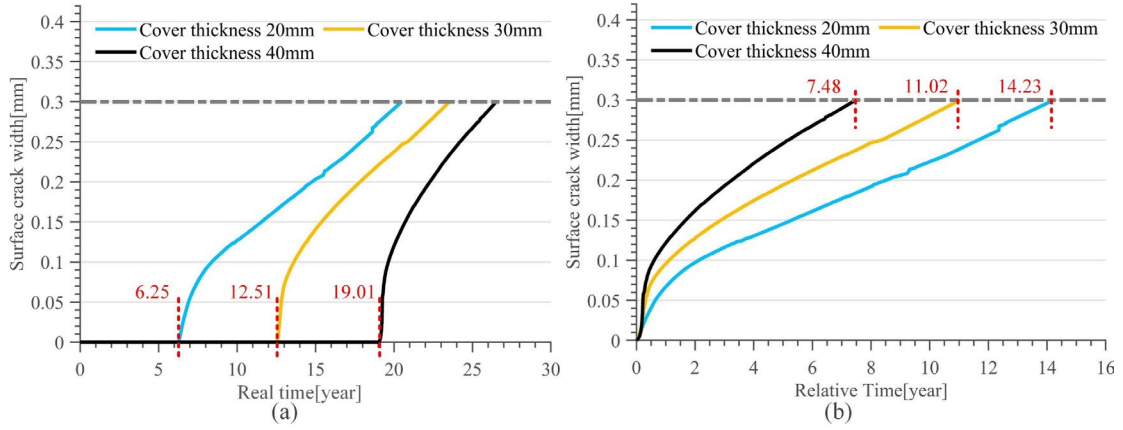621　C=30mm; (c) C=40mm.

622

Fig. 17. Time-surface crack width curves for different cover thicknesses: (a) real time; (b) time relative to surface crack initiation.

Fig. 17 shows the relationships between the exposed time and the surface crack width for different cover thicknesses. For 20 mm, 30 mm and 40 mm cases, the corresponding surface cracks appear after 6.25, 12.51 and 19.01 years, indicating a significant influence of cover thickness on the corrosion. Fig. 17(b) shows the relationship between relative time, the time after the surface crack initiation, and the surface crack width. The time from surface crack initiation to reaching the critical width is 7.48 years, 11.02 years, and 14.23 years for cover thickness $C = 20$mm, $C = 30$mm and $C = 40$mm. In summary, the corrosion analyses show that a thicker concrete cover can delay the time of surface crack initiation. On the other hand, it may accelerate the corresponding crack opening rate and result in a lower load-bearing capacity of the RC structure given the same structural dimensions. Therefore, an optimal cover thickness under specified loading and environmental conditions may be determined to balance the safety and serviceability requirements by combing the proposed modeling framework with an appropriate optimization algorithm.
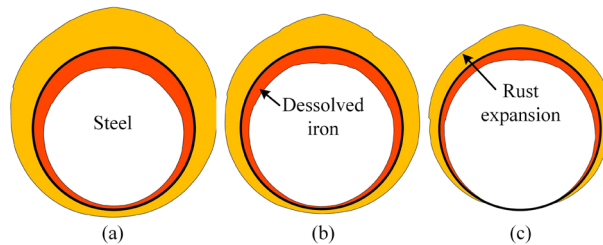

Fig. 18. Shape of the corroded rebars at critical crack width for the cover thickness of (a) 20mm, (b) 30mm, and (c) 40mm. (Deformation scale factor: 10)

644　　　Fig. 18 shows the shape of the corroded rebars for different cover thicknesses when crack width

645　　reaches its critical value. Red and yellow regions represent the dissolved iron and the accumulated

646　　rust product, and a deformation scale factor of 10 is adopted for better illustration. It can be clearly

647　　observed that when the surface crack reaches the critical width, the corrosion degree (steel loss ratio)

648　　for thinner cover thickness is bigger, indicating that the thinner cover thickness case experienced

649　　longer corrosion time from crack surface initiation to reaching the critical value. This observation

650　　is consistent with the surface crack width curves depicted in Fig. 17.

651　　　Fig. 19 shows the relationships between the corrosion current density and the exposure time at

652　　different locations on the rebar surface. It can be observed that at $\theta = 0$ and $\theta = \pi/2$, the

653　　corrosion current densities show a sharp increase, then decrease gradually. While at location $\theta = \pi$

654　　the corrosion current densities become constant values after sharp increases, indicating that at this

655　　time the corrosion process is mainly dominated by the micro-cell corrosion mechanism. In addition,

656　　comparisons between different thickness cases show that the steady corrosion current density
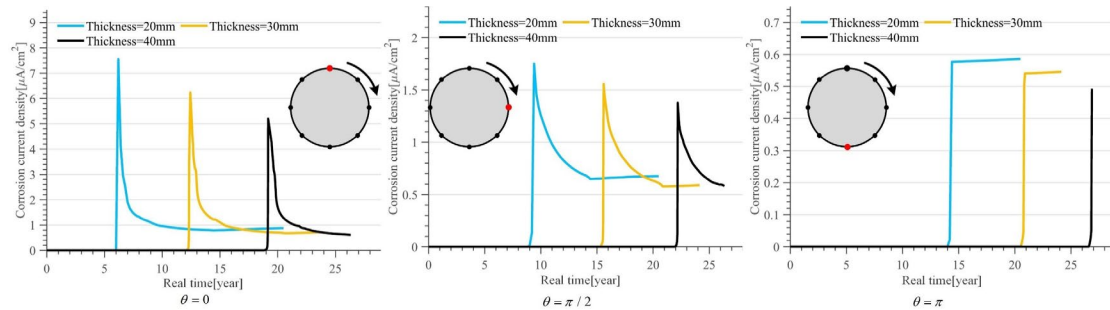
657　　decreases with the increase of the cover thickness.

658

659

660　　　　Fig. 19. Corrosion current densities at different locations with different cover thicknesses.

661

662　4.3. Influence of relative humidity on the corrosion-induced fracture

663　Section 2 shows that the relative humidity considerably affects all the mass transport processes, i.e.,

664　the transport of moisture, chloride and oxygen. Hence, this section considered three relative

665　humidity cases: 50%, 70% and 90%. It should be noted that the 50% relative humidity is out of the

666　humidity range of the experimental results used for determining the oxygen diffusivity (Eq. (20).

667　However, Eq. (20) is a monolithic function of humidity. It is assuming that it still can reflect some

668　characteristics of the oxygen diffusivity change out of the experimental relative humidity range. Fig.

669　20 depicts the relationships between the surface crack width and the exposure time of different

670　relative humidity cases. It can be seen that the relative humidity significantly affects the surface

671　crack initiation time. For 50%, 70% and 90% humidity cases, the cracks initiate at the 49.53th year,

672　12.51th year and 5.48th year. Fig. 20(b) shows that for the lowest relative humidity case (h=50%),

673　the period from surface crack initiation to reaching the critical width is about 2.93 years, much

674　shorter than that of the other cases. And the surface crack width curve of 50% relative humidity is

675　quite different from the other two cases. This may be caused by the highly localized rust

676　accumulation, as shown in Fig. 21(a). It shows that in the case of 50% relative humidity, only about

677　one-quarter of the rebar surface is corroded. In addition, the rust layer has two sharp corners near

678　the corrosion-induced cracks. In contrast, the corrosion for 90% relative humidity is rather uniform,

679　as shown in Fig. 21(c). Because higher humidity leads to bigger diffusion coefficients and higher

680　oxygen access, which will accelerate the depassivation process. The corresponding corrosion

681　current densities for different humidity cases are depicted in Fig. 22. It can be seen that the corrosion

682　current density distributions are consistent with the corrosion shapes shown in Fig. 21.
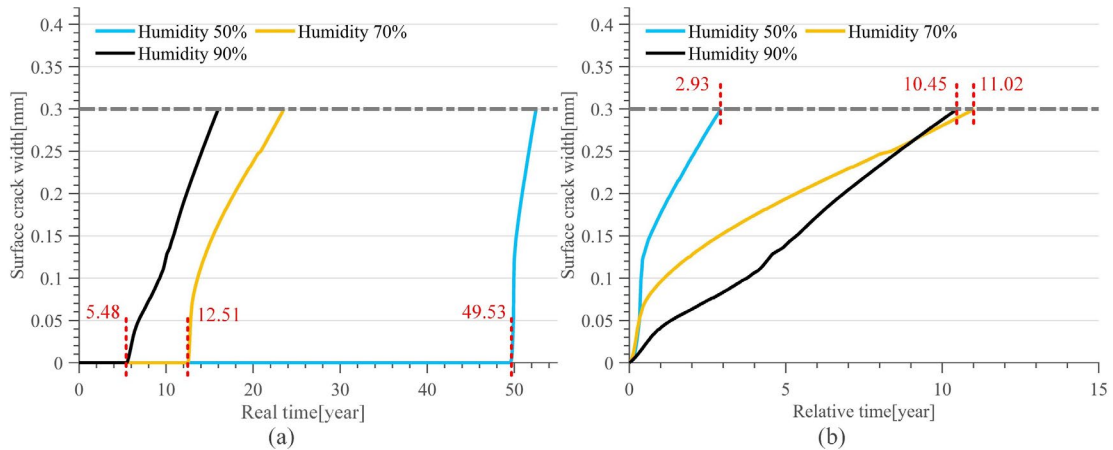
683

684
685　Fig. 20. Time-surface crack width curves for different humidity cases: (a) real time; (b) time
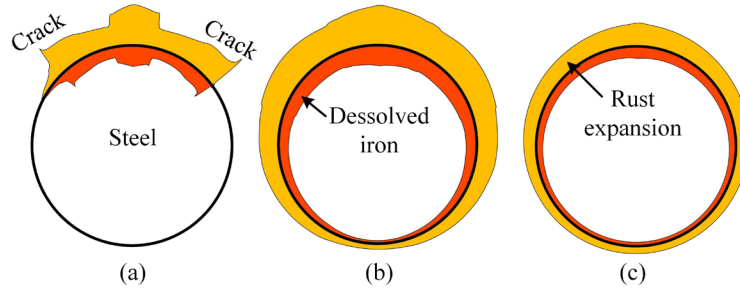686　relative to surface crack initiation.

687

Fig. 21. Corrosion shapes of the rebars for humidity cases at critical crack width: (a) 50%; (b) 70%; (c) 90%. (Deformation scale factor: 10)
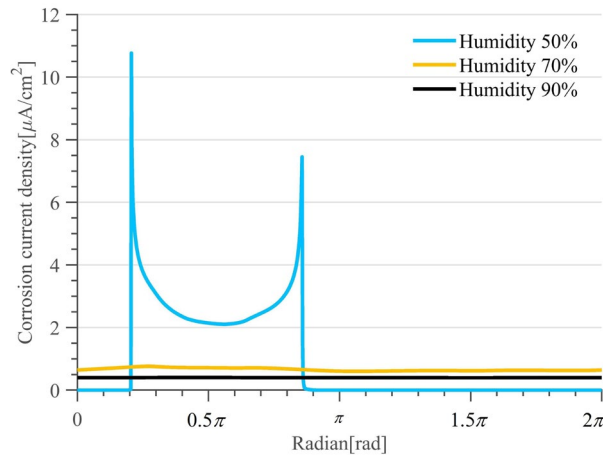

Fig. 22. Corrosion current densities for different humidity cases at the critical crack width.

The predicted crack patterns for different humidity cases are depicted in Fig. 23. It can be observed that the crack patterns of 50% and 70% cases are similar to each other. For the 90% case, the crack pattern is very different. It can be seen from Fig. 23(c) that the side cracks are located near the bottom of the rebar, and additional microcracks initiate near the rebar surface. This different crack pattern is actually caused by the relatively uniform corrosion as shown in Fig. 21(c), where the mortar around the rebar is subjected to a relatively uniform hoop stress.
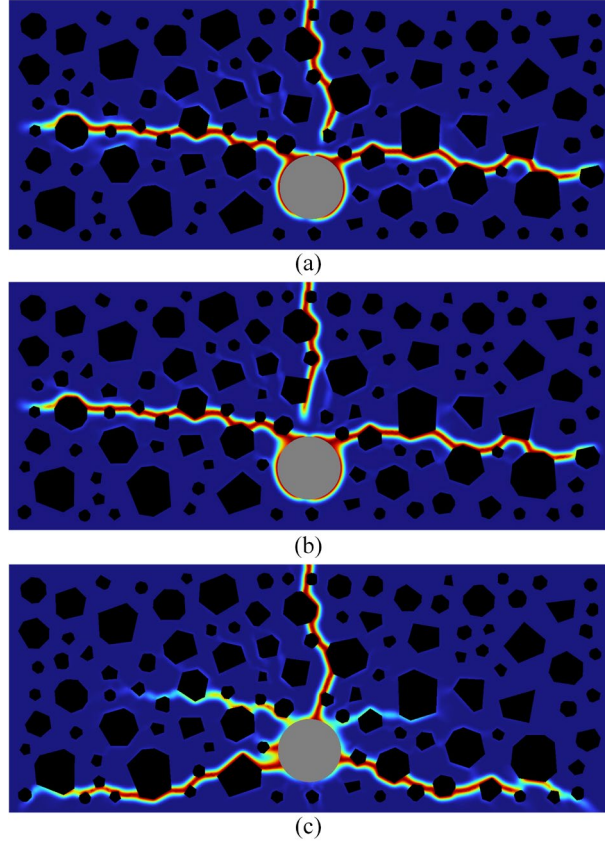
(a)

(b)

(c)

Fig. 23. Crack patterns for different relative humidity cases at the critical crack width: (a) 50%; (b) 70%; (c) 90%.

4.4. Influence of temperature on the corrosion induced fracture

As shown in sections 2 and 2.2, temperature can affect both the mass transport and the electrochemical reactions. In order to investigate the influence of the temperature on the entire corrosion process, three different temperatures were considered, i.e., $T=20^{\circ}C$, $T=30^{\circ}C$ and $T=40^{\circ}C$. As suggested by Pour-Ghaz et al. (2009a), the temperature also affects the amount of oxygen that is dissolved in water, and the effect can be evaluated by

$$\ln C_{O_2}^s = -139.344 + \frac{1.575 \times 10^5}{T} - \frac{6.642 \times 10^7}{T^2} + \frac{1.244 \times 10^{10}}{T^3} - \frac{8.622 \times 10^{11}}{T^4} \tag{91}$$

where $C_{O_2}^s$ is the oxygen concentration in the pore solution at the concrete surface (mg/L). Fig. 24 shows the predicted crack patterns and corrosion shapes of different temperatures. It can be observed that the temperature significantly affects the crack patterns and the corrosion shapes. For the cases of $T=20^{\circ}C$ and $T=30^{\circ}C$, the crack patterns are quite similar. For $T=40^{\circ}C$ two additional radial cracks initiates at the bottom of the rebar surface, behaving more like a uniform corrosion fracture pattern.

36

717   The corresponding corrosion shape in Fig. 24 suggests that higher temperature does not necessarily
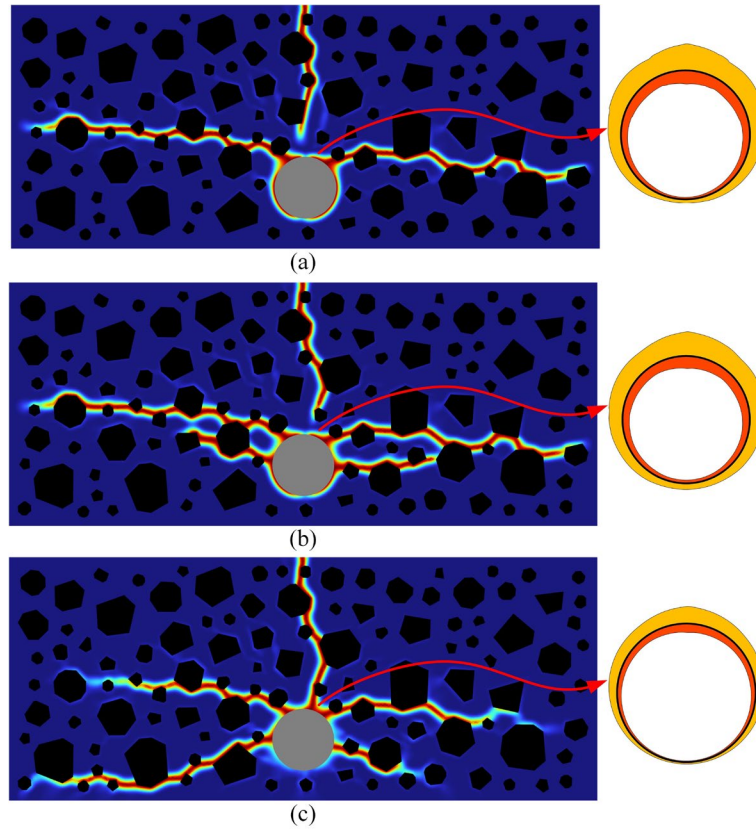
718   lead to a bigger steel loss ratio.

719

(a)

(b)

(c)

720

721   Fig. 24. Crack patterns for different temperatures at the critical crack width: (a) 20°C; (b) 30°C; (c)
722   40°C.

723

724   Fig. 25(a) shows the relationships between the surface crack width and the exposed time of

725   different temperatures. It can be seen that higher temperature can accelerate the onset of the surface

726   cracks, that the surface crack initiation time for 20°C, 30°C and 40°C are 14.2th year, 8.87th year

727   and 5.86th year, respectively. The crack surface width versus relative time curves in Fig. 25(b)

728   shows that it takes longer time to reach the critical crack width in case of a lower temperature. The

729   average corrosion current densities of different temperatures are shown in Fig. 26. It can be clearly

730   observed that the steady corrosion current density increases with the temperature in the current

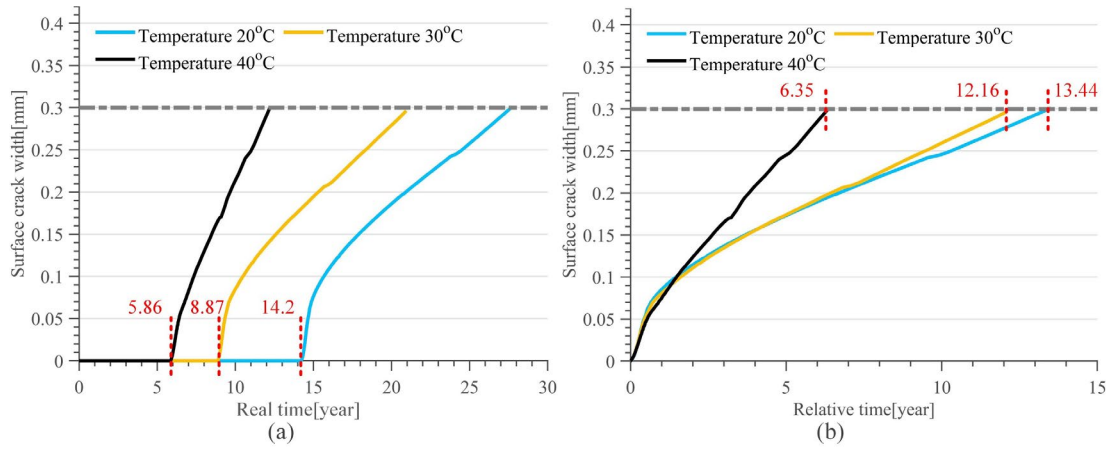731   simulation, supporting that the higher temperature leads to less time to reach the critical crack width.

732

733

734 Fig. 25. Time-surface crack width curves for different temperatures: (a) real time; (b) time relative
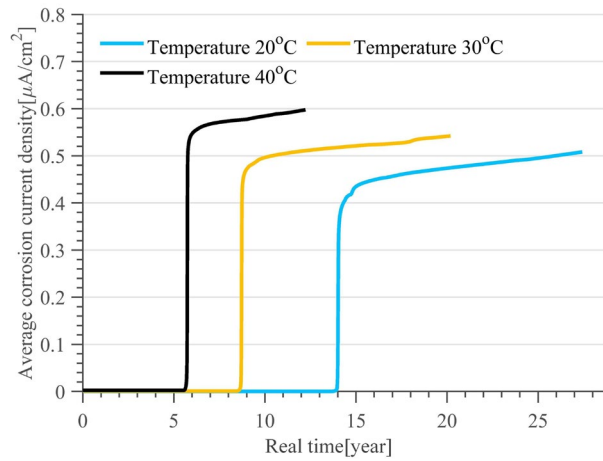735 to surface crack initiation.

736

737

738 Fig. 26. Average corrosion current curves of different temperatures after surface crack initiation.

739

740 **5. Conclusions**

741 In this paper, a fully coupled electro-chemo-mechanical phase field method is established to
742 simulate the entire corrosion process of RC structures. In the modeling, the non-mechanical
743 processes (mass transport and electrochemical corrosion) and the mechanical behavior (damage) are
744 coupled together at meso-scale. Modified crack direction-dependent diffusion coefficient tensors
745 are proposed to implement the effect of damage on the transport of moisture, chloride and oxygen
746 in concrete. Experimental results of a RC beam containing four rebars are simulated to verify the
747 proposed method, showing the ability to conduct high-fidelity simulations of corrosion-induced
748 fracture in RC structures. Based on the simulations, the following conclusions can be reached:

38

749　(1) The aggregate distribution in concrete significantly influences the mass transport process and

750　　　the damage evolution, leading to variable crack initiation time and the time required for the

751　　　crack to reach critical width. However, the major influence is observed in time when the crack

752　　　reaches the critical width. The simulations show that the time can vary by about 20% with

753　　　different aggregate distributions.

754　(2) Thicker concrete cover thickness can delay the onset of surface cracks. However, it will lead to

755　　　a more rapid increase of the crack width after initiation and a shorter time from surface crack

756　　　initiation to reaching the critical value.

757　(3) Higher relative humidity will accelerate the depassivation process, resulting in the early onset

758　　　of surface cracks. In addition, with the faster depassivation of the rebar surface, the rebar will

759　　　show a relatively uniform corrosion shape.

760　(4) The temperature has a clear influence on the corrosion shape of the rebar as well as the

761　　　corresponding crack pattern. Higher temperatures can accelerate the initiation and propagation

762　　　of corrosion on the rebar surface.

763

Acknowledgements

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