# Energy efficiency evaluation for water supply systems in tall buildings 

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#### Abstract

High-rise housing, a trend in densely populated cities around the world, increases energy use for water supply and corresponding greenhouse gas emissions. With emphasis on improving energy efficiency in water supply systems, this paper proposes an energy efficiency evaluation measure for water supply system designs and demonstrates its potential applications in a typical high-rise water supply system. In the proposed measure, energy efficiency in a water supply system is defined as the potential energy required at the demand locations divided by the pumping energy of the supply system. The outcome of this paper provides useful benchmark references for not only water supply system designs but also water demand management programmes in buildings.


Practical application: An energy efficiency evaluation measure for water supply system designs is used to establish benchmark references for not only water supply system designs but also water demand management programmes in buildings.

## Keywords

Water supply, high-rise buildings, energy efficiency, benchmarks

## Introduction

The water supply network is the largest single energy consumer in a city. ${ }^{1}$ It was reported that in some developed cities, $40 \%$ of pumping energy is consumed inside buildings. ${ }^{2,3}$ Improving energy efficiency of water supply systems in buildings is a way of reducing carbon emissions. ${ }^{3}$

In high-rise buildings, gravity storage tanks on the rooftops (or on intermediate mechanical floors) are designed for distributing water through down-feed pipes. ${ }^{4,5}$ Pressure reducing valves (PRV) with adjustable settings and screwed joints are commonly installed to minimize the problems of water leakage or damages in the supply pipes and appliances caused by excessive water pressure on lower floors in low demand situations. In fact, pressurization that requires excessive energy or water pressure in a water supply system is a waste of energy.

Currently in Hong Kong, the average residential building height is estimated to be 26 storeys. ${ }^{3}$ In response to the call for sustainable building designs, an energy efficiency evaluation measure, verified with measurements performed in some high-rise residential buildings in Hong Kong, has been proposed for designing water supply systems in buildings. ${ }^{6}$ It was demonstrated that by relocating water storage tanks and avoiding overpressure at water demand points, energy efficiency of some high-rise water supply systems could be as high as 0.34 (the existing range is $0.20-0.25$ ). To improve water
supply system performance, reducing friction in the supply pipes can be another significant contributor. ${ }^{7}$

## [Insert Figure 1]

## Methodology

Energy efficiency of a water supply system in high-rise buildings, which can be determined using the system heights (as shown in Figure 1), pipe friction and allowable pressure head, is defined as the potential energy required at the demand locations $E_{\text {out }}$ divided by the pumping energy of the supply system $E_{\text {pump, }}{ }^{8}$

$$
\begin{equation*}
\alpha=\frac{E_{\text {out }}}{E_{\text {pump }}} \tag{1}
\end{equation*}
$$

$E_{\text {out }}(\mathrm{MJ})$ is the potential energy for volumetric water demands $v_{i}$ at height $h_{i}$ as given below, where $\rho\left(=1000 \mathrm{kgm}^{-3}\right)$ is the water density and $g\left(=9.81 \mathrm{~ms}^{-2}\right)$ is the gravitational force,

$$
\begin{equation*}
E_{\text {out }}=\rho g \sum_{i=1}^{n} v_{i} h_{i} \tag{2}
\end{equation*}
$$

Pumping energy of lifting water from the break tank to the roof tank $E_{\text {pump }}(\mathrm{MJ})$ is defined in Equation (3), where $\eta_{c}$ is the design overall transmission efficiency; $h_{l}$ is the height difference between the break tank water surface and the roof tank inlet, which is also the sum of the height measured from the roof tank base to the tank inlet $h_{c}$, the height
difference between the demand $n$ and the tank base $h_{b}$, and the height difference between the break tank water surface and the top demand location $h_{n}$; and $H_{o}$ is the desired minimum water pressure head assumed at the roof tank inlet. $H_{f}$, the friction head required in the up-feed water pipe, is given by Equation (4), where $f$ is the friction factor, $u\left(\mathrm{~ms}^{-1}\right)$ is the flow velocity, $d(\mathrm{~m})$ is the hydraulic diameter and $L_{e}$ is the pipe equivalent length taking all pipe fittings into account. ${ }^{5}$

$$
\begin{align*}
& E_{\text {pump }}=\frac{\rho g\left(h_{l} \sum_{i=1}^{n} v_{i}+H_{f}+H_{o}\right)}{\eta_{c}} ; h_{l}=h_{c}+h_{b}+h_{n}  \tag{3}\\
& H_{f}=f \frac{u^{2}}{2 g d} L_{e} \tag{4}
\end{align*}
$$

It is noted that the design overall transmission efficiency $\eta_{c}$ (34-65\%) accounts for 50$80 \%$ of the pump efficiency $\eta_{p}$, about $90 \%$ of the mechanical transmission efficiency $\eta_{m}$ and $70-90 \%$ of the electric motor efficiency $\eta_{e}{ }^{9,10}$

$$
\begin{equation*}
\eta_{c}=\eta_{p} \eta_{m} \eta_{e} \tag{5}
\end{equation*}
$$

The pump power $P_{t}(\mathrm{~kW})$ is given by,

$$
\begin{equation*}
P_{t}=\frac{q_{o}\left(H_{f}+H_{o}\right)}{100 \eta_{c}} \tag{6}
\end{equation*}
$$

By assuming a mass balance on the roof tank, the following equation can be used to determine the inflow rate of up-feed pipe $q_{o}\left(\mathrm{Ls}^{-1}\right)$ required to fulfil a time variant water
demand $q_{w}\left(\mathrm{Ls}^{-1}\right)$ within the time period of demand $\tau_{\infty}$, where $V_{\infty}(\mathrm{L})$ is the total volumetric water consumption, ${ }^{11}$

$$
\begin{equation*}
V_{\infty}=\int_{\tau_{\infty}} q_{w} d t \leq q_{o} \tau_{\infty}+V_{o} ; \quad \tau_{\infty}=t_{\infty}-t_{0} \tag{7}
\end{equation*}
$$

There are solution pairs ( $V_{o}, q_{o}$ ) to Equation (7) at any time period within the time period of demand, $\tau_{o} \in \tau_{\infty}$.

$$
\begin{equation*}
V_{o}=\max \left\{\int_{\tau_{o}}\left(q_{o}-q_{w}\right) d t\right\} \tag{8}
\end{equation*}
$$

The required inflow rates for the minimum storage tank volume $\left(V_{o}=0\right)$ and the maximum storage tank volume $\left(V_{o}=V_{\infty}\right)$ are $q_{o}=\max \left(q_{w}\right)$ and $q_{o}=q_{o, \infty}$ respectively,

$$
q_{o}=\left\{\begin{array}{rc}
\max \left(q_{w}\right) ; & V_{o}=0  \tag{9}\\
q_{o, \infty} ; & V_{o}=V_{\infty}
\end{array} ; q_{o, \infty}=\frac{V_{\infty}}{\tau_{\infty}}\right.
$$

The required inflow rate $q_{0, \infty}<q_{o}<\max \left(q_{w}\right)$ is dependent on the storage tank volume in terms of the water demand over any integration time period $\tau_{o}(\mathrm{~s})$,

$$
\begin{equation*}
q_{o}=\frac{V_{o}}{\tau_{0}} \tag{10}
\end{equation*}
$$

The water demand $q_{w}\left(\mathrm{Ls}^{-1}\right)$ is defined by a number of water appliances (i.e. $\left.1,2, \ldots, k\right)$ operating at any time $t \in \tau_{\infty}$,

$$
\begin{equation*}
q_{w}=\sum_{k} q_{c, k}(t) \tag{11}
\end{equation*}
$$

Taking a flushing water system as an example, the demand period $t \in \tau_{w, l}$ (zero demand otherwise) is determined from the cistern demand flow rate $q_{c}\left(\mathrm{Ls}^{-1}\right)$ and cistern flushing volume $V_{c}(\mathrm{~L}) . q_{c}$ and $V_{c}$ can be obtained from distribution functions $q_{c} \in \tilde{q}_{c}$ and $V_{c} \in \tilde{V}_{c}$ via the Monte-Carlo sampling technique. $\vartheta \in[0,1]$, a random number between 0 and 1 taken from a pseudo-random number set generated by a prime modulus multiplicative linear congruential generator, is expressed by, ${ }^{12,13}$

$$
\begin{equation*}
\vartheta=\int_{-\infty}^{q_{c}} \tilde{q}_{c} d q ; \vartheta=\int_{-\infty}^{V_{c}} \tilde{V}_{c} d V ; \quad \tau_{w, l}=\frac{V_{c}}{q_{c}} \tag{12}
\end{equation*}
$$

Operation of an appliance is random within a time period $\tau_{w}(\mathrm{~s})$ which starts at time $t_{w, 0}$ (s) and ends at time $t_{w, \infty}$ (s); it equals to the sum of time periods of non-zero demands $\tau_{\omega, l}$ (s) and zero demands $\tau_{0, l}(\mathrm{~s})$ for $l=1,2, \ldots, N_{a}$, where $N_{a}\left(\mathrm{~h}^{-1}\right)$ is the hourly demand of an appliance within the time period and the time periods are represented by the appliance demand start time $t_{w 1, l}(\mathrm{~s})$ and the appliance demand end time $t_{w 2, l}(\mathrm{~s}),{ }^{11}$

$$
\begin{align*}
& \tau_{w}=t_{w, \infty}-t_{w, 0} \\
& = \begin{cases}\tau_{0,1}+\tau_{w, 1}+\tau_{0,2}+\tau_{w, 2}+\cdots+\tau_{0, l}+\tau_{w, l}+\cdots+\tau_{0, N_{a}}+\tau_{w, N_{a}}+\tau_{0, N_{a}+1} \\
\tau_{w, 0}+\tau_{0,1}+\tau_{w, 1}+\tau_{0,2}+\tau_{w, 2}+\cdots+\tau_{0, l}+\tau_{w, l}+\cdots+\tau_{0, N_{a}}+\tau_{w, N_{a}}-\tau_{0, N_{a}+1} & ; \\
t_{w 2, N_{a}} \leq t_{w, N_{a}}>t_{w, \infty}\end{cases} \tag{13}
\end{align*}
$$

$$
\begin{align*}
& \tau_{0, l}=t_{w 1,1}-t_{w 2, l-1} ; \quad \tau_{w, l}=t_{w 2, l}-t_{w 1, l}  \tag{14}\\
& \tau_{0,1}=\left\{\begin{array}{l}
t_{w 1,1}-t_{w, 0} ; \\
t_{w 1,1}-t_{w 2,0}
\end{array} \quad \tau_{0, N_{a}+1}=\left\{\begin{array}{ll}
t_{w, \infty}-t_{w 2, N_{a}} \\
t_{w 2, N_{a}}-t_{w, \infty}=t_{w 2,0}-t_{w, 0}=\tau_{w, 0}
\end{array} ; \begin{array}{l}
t_{w 2, N_{a}} \leq t_{w, \infty} \\
t_{w 2, N_{a}}>t_{w, \infty}
\end{array}\right.\right. \tag{15}
\end{align*}
$$

The demand start time $t_{w 1, l}(\mathrm{~s})$ is given by a randomly distributed fractional demand start time $\hat{t}_{\text {w1,l }}(\mathrm{s})$ and can be determined via Monte Carlo simulations using a uniformly distributed fractional demand start time $U(\mathrm{~s})$,

$$
\begin{equation*}
t_{w 1, l}=\hat{t}_{w 1, l} \tau_{w} ; \vartheta=\int_{-\infty}^{\hat{t}_{w, 1}} U d t \tag{16}
\end{equation*}
$$

The hourly demand $N_{a}\left(\mathrm{~h}^{-1}\right)$ of an appliance is given by the following equation, where $n_{a}$ (person ${ }^{-1} \mathrm{~h}^{-1}$ ) is the hourly demand per person, $N_{p}$ (persons) is the number of persons at a time expressed through an occupant load variation factor $\phi(t)$, and $N_{p, \max }$ (persons) is the maximum occupant load of appliance designated for serving an apartment floor area $A_{f}\left(\mathrm{~m}^{2}\right)$ and determined via the occupant-area ratio $O_{a}\left(\right.$ person $\left.\mathrm{m}^{-2}\right),{ }^{14}$

$$
\begin{equation*}
N_{a}(t)=n_{a} N_{p}(t)=n_{a} N_{p, \max } \phi(t)=n_{a} O_{a} A_{f} \phi(t) \tag{17}
\end{equation*}
$$

Figures 2 and 3 exhibit the per-person hourly usage patterns and occupant load variations of a residential water closet (WC) respectively. The hourly demand $N_{a}$ for each WC serving $N_{p, \max }=4.2$ persons is shown in Figure 4. ${ }^{14,15}$

## [Insert Figure 2]

## [Insert Figure 3]

## [Insert Figure 4]

## [Insert Figure 5]

## Simulations

As appliance operations is random, the time series of demand flow rates $q_{w}(t)$ was simulated using Equation (11) in terms of maximum and minimum daily volumetric consumption $\int_{\tau_{\infty}} q_{w} d t$ for 100 years operations of the water supply system. The simulation results are shown in Figure 5, with input parameters in Figures 1-4 using Equations (13)-(17) via the Monte-Carlo sampling technique described by Equation (12). The procedures were coded and executed in an i7 machine, and the executing time was about one week per simulation case. Results in Figure 5(a)\&(b) indicated that the simulated daily consumption range was $76.1 \mathrm{~m}^{3} \mathrm{~d}^{-1}$ to $81.9 \mathrm{~m}^{3} \mathrm{~d}^{-1}$, with an average of $78.9 \mathrm{~m}^{3} \mathrm{~d}^{-1}$ calculated from all simulation days.

Figure 6(a) illustrates the solution pairs ( $V_{o}, q_{o}$ ) given by Equation (10) for the demand time series shown in Figure 5(a) with respect to demand periods $\tau_{o}=1,60$ and 300s. The results showed that a coarse integration time period $\tau_{o}$ (e.g. 300s) for the simulation may not give an accurate solution for small storage volume, however, no significant difference was found for the simulation results among integration demand periods $\tau_{o}=1,10$ and 60 s as shown in Figures 6(a)\&(b). Some differences in range of small storage volume was found for longer integration demand time period of 300s as demonstrated in Figure 6(a). At a minimum storage volume of 250 L (Hong Kong practice), the simulated inflow rates were from 1.907 to $1.924 \mathrm{Ls}^{-1}$ for Figure 5(a) and equalled to $1.76 \mathrm{Ls}^{-1}$ for Figure 5(b).

These inflow rates do not pose significant practical concerns about specifying the inflow rates required for general engineering applications as safety margins are normally imposed when selecting a water pump to feed the storage tank. The minimum flow rates for the cases shown in Figures 6(a) and 6(b) were $0.95 \mathrm{Ls}^{-1}$ and $0.88 \mathrm{Ls}^{-1}$ respectively.

## [Insert Figure 6]

## Illustration applications

As the water pressure head at the government water mains in Hong Kong is insufficient to reach the topmost appliances in almost all high-rise buildings, gravity storage tanks on building rooftops (or on intermediate mechanical floors) are commonly designed for distributing water through down feed pipes. ${ }^{8}$ An example of high-rise tank water supply system for 600 residential WC cisterns is presented in Table $1 .{ }^{16}$ Design inflow rates were determined for the design and installed conditions and then compared with cases using some existing design practices. ${ }^{5}$ As the design inflow rate under the installed conditions allowed a much greater margin of safety (of $30 \%$ ) than the one under the design conditions, a larger pump was selected for the installed system. In the base case, the roof tank was fed by a pump at the design flow rate through a 67 -mm-diameter pipe. The total static head for $h_{l}=100 \mathrm{~m}$ was counted and a friction head loss $H$ for an equivalent pipe length $h_{f_{0}}=150 \mathrm{~m}$ was included. To determine the system efficiencies, an average height
of demand locations $h_{d}=50 \mathrm{~m}$ and an overall pump efficiency $\eta_{c}=0.5625$ were applied. Equation (1) becomes,

$$
\begin{equation*}
\alpha=\frac{H_{d} \eta_{c}}{H_{f o}+h_{l}} \tag{18}
\end{equation*}
$$

To determine the pumping energy, Equation (19) was used.

$$
\begin{equation*}
E_{\text {pump }}=\frac{\rho g V\left(H_{f o}+h_{l}\right)}{\eta_{c}} \tag{19}
\end{equation*}
$$

Table 1 shows that system efficiency of the installed system decreased from 0.243 (design value) to 0.235 , corresponding to an efficiency drop of $3 \%$ or an extra energy consumption of 3.1\%. It is the result of a higher friction head loss in the pipelines caused by a higher water velocity than the design value.

Table 1. An example of high-rise tank water supply system for 600 residential WC cisterns

| Parameters | Roof-tank system (Design) | Roof-tank system (Installed) | Variable speed pumping system | Intermediate-and-rooftank system |
| :---: | :---: | :---: | :---: | :---: |
| Total tank size (m ${ }^{3}$ ) | 0.25-27 | 0.25-27 | 0.25-27 | 0.5-27 |
| Daily consumption ( $\mathrm{m}^{3}$ ) | 76-82 | 76-82 | 76-82 | 76-82 |
| Design inflow rate ( $\mathrm{Ls}^{-1}$ ) | 5.1 | 6.6 | 0.95-1.9 | 3.2 |
| Base case* |  |  |  |  |
| Feed pipe water velocity ( $\mathrm{ms}^{-1}$ ) | 1.5 | 1.9 | 0.3-0.5 | 0.9 |
| Friction head loss (m) | 16.0 | 19.6 | 10.4-11.2 | 11.4-12.7 |
| System efficiency | 0.243 | 0.235 | 0.253-0.255 | 0.302 |
| Total electricity power (kW) | 10.5 | 14.1 | 1.9-3.8 | 9.9 |
| Daily pumping energy (kWh) | 43-46 | 44-48 | 41-44 | 32-35 |
| Case A: Exit static head reduced by 50\% |  |  |  |  |
| Feed pipe water velocity (ms ${ }^{-1}$ ) | 1.5 | 1.9 | 0.3-0.5 | 0.9 |
| Friction head loss (m) | 11.0 | 14.6 | 5.4-6.2 | 6.4-7.7 |
| System efficiency | 0.253 | 0.245 | 0.265-0.267 | 0.321 |
| Total electricity power (kW) | 10.1 | 13.5 | 1.8-3.6 | 9.3 |
| Daily pumping energy (kWh) | 41-44 | 42-46 | 39-42 | 30-33 |
| Case B: Building height increased by 50\% |  |  |  |  |
| Feed pipe water velocity ( $\mathrm{ms}^{-1}$ ) | 1.5 | 1.9 | 0.3-0.5 | 0.9 |
| Friction head loss (m) | 19.0 | 24.4 | 20.6-11.8 | 12.0-14.1 |
| System efficiency | 0.250 | 0.242 | 0.261-0.263 | 0.314 |
| Total electricity power (kW) | 15.3 | 20.6 | 2.7-5.5 | 14.3 |
| Daily pumping energy (kWh) | 62-67 | 64-69 | 59-64 | 46-50 |
| Case C: Supply pipe diameter one size down (i.e. 54 mm ) |  |  |  |  |
| Feed pipe water velocity ( $\mathrm{ms}^{-1}$ ) | 2.2 | 2.9 | 0.4-0.8 | 1.4 |
| Friction head loss (m) | 27 | 34 | 10.9-13.0 | 13.4-16.8 |
| System efficiency | 0.222 | 0.210 | 0.249-0.254 | 0.292 |
| Total electricity power (kW) | 11.5 | 15.8 | 1.9-3.8 | 10.3 |
| Daily pumping energy (kWh) | 47-50 | 49-53 | 41-45 | 33-36 |

[^0]To achieve the design flow rate, variable speed control is a solution. Based on the mass balance assumption presented in the previous section, the relationship between inflow rate to the tank and size of the tank determined for the usage patterns is graphed in Figure 6. Taking a daily consumption range from $76 \mathrm{~m}^{3}$ to $82 \mathrm{~m}^{3}$, the design flow rate is from $0.95 \mathrm{~L} / \mathrm{s}$ (at a tank size of $27 \mathrm{~m}^{3}$ ) to $1.9 \mathrm{~L} / \mathrm{s}$ (at a tank size of $0.25 \mathrm{~m}^{3}$ ) for fulfilling the water demands in some residential buildings. ${ }^{9}$ As the efficiency of a variable speed pumping system can be increased to 0.255 , corresponding to $5.1 \%$ pumping energy savings compared with the design system, energy loss due to system friction in high-rise pumping can be significant and system friction optimization should not be ignored in the future designs of tank water supply network.

Zoning a high-rise water supply system by an intermediate tank can limit the system pressure and thus reduce the pumping energy. As exhibited in Table 1, the efficiency of an intermediate-and-roof tank system can be as high as 0.302 , corresponding to $24 \%$ pumping energy savings.

In contrast to the base-case scenario, three cases namely A, B and C are illustrated in Table 1 to demonstrate the effects of different design values on system efficiency with graphically illustrated in Figure 7.

In Case A, the exit static head loss of the roof tank inlet was reduced by $50 \%$ at the same supply flow rate. Energy loss reduction was represented by a system efficiency drop from $6.2 \%$ in the base case to $4.4 \%$ in this case.

For Case B, a building which was $50 \%$ taller than the one in the base case was employed under the same water supply design conditions. In this case, the exit friction head loss did not increase proportionally with the building height, and the system efficiency increased slightly as compared to the base case. Therefore, at the same supply flow rate, potential energy savings can be achieved by using water appliances with low pressure loss.

Case C was a water supply system with a smaller up-feed pipe, one size down from 67 mm to 54 mm in diameter. Significantly increased friction loss in the pipe resulted in $8.3 \%$ system efficiency drop under the design conditions or $10.7 \%$ under the installed conditions, as compared to the base case. A less significant influence on the intermediate-and-roof tank system, where the design flow rate was lower, was found (-3.4\%). Less impact on energy efficiency (from $-0.5 \%$ to $-1.6 \%$ ) was also shown for the intermediate-and-roof tank system. Although the total storage volume remains unchanged, it is noted that additional intermediate tank with separate pump sets require additional cost. The installation would be cost justified with short payback periods. ${ }^{17}$

## [Insert Figure 7]

## Conclusion

With emphasis on improving energy efficiency in water supply systems, this paper proposed an energy efficiency evaluation measure for water supply system designs and demonstrated its potential applications in a typical high-rise water supply system. In the proposed measure, energy efficiency in a water supply system is defined as the potential energy required at the demand locations divided by the pumping energy of the supply system. The outcome of this paper provides useful benchmark references for not only water supply system designs but also water demand management programmes in buildings.

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Figure 6. Solutions of inflow rate and storage volume for the minimum and maximum demand time series

Figure 7. Summary of system efficiencies


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Figure 2. Per-person hourly WC demand $n_{a}$


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Figure 6. Solutions of inflow rate and storage volume for the minimum and maximum demand time series


Figure 7. Summary of system efficiencies


[^0]:    * Base case: Building height = 100 m ; Exit static head loss = 10 m ; Feed pipe = 67 mm in diameter,
    with an equivalent length of 1.5 times the building height.

